

Balances on Multiple Units

(No reaction)

Prof. Faith Morrison

Department of Chemical Engineering Michigan Technological University

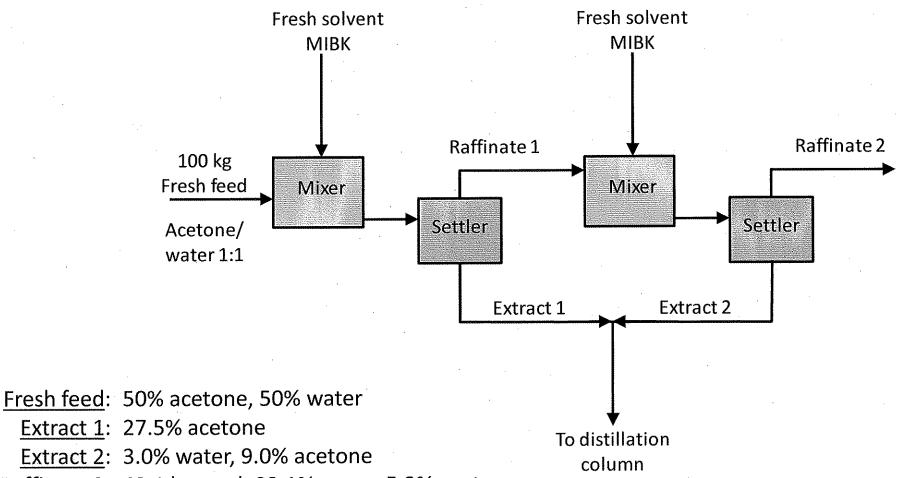
28 May 2013

YouTube: DrMorrisonMTU

Reference: Felder and Rousseau, 3rd Edition, 2000



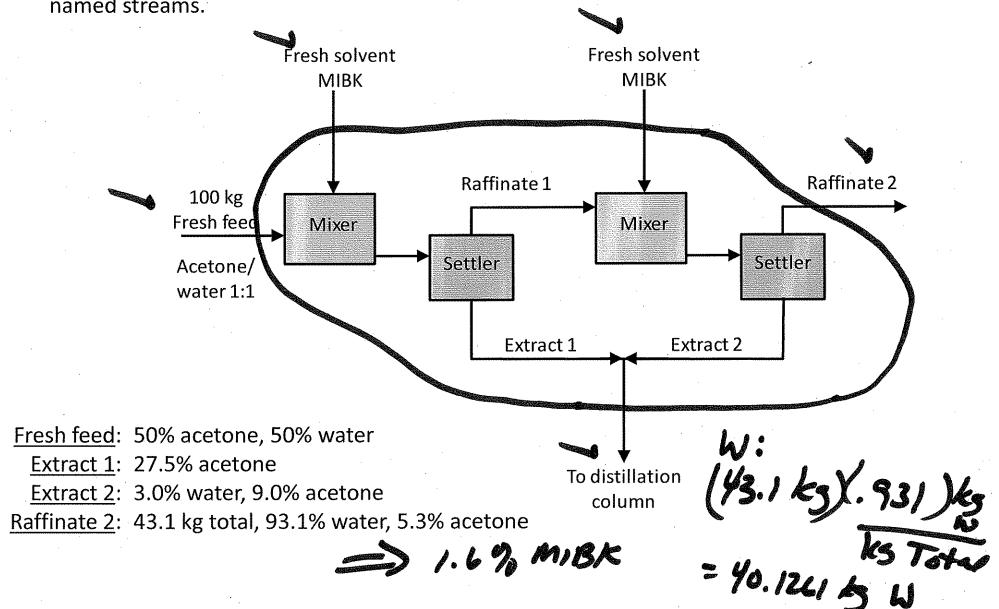
FR Example 4.4-2 (partial): The two-stage extraction process shown below is used to separate a 50/50 wt% mixture of acetone and water. The extraction solvent is methyl isobutyl ketone (MIBK). For every 100 kg of fresh feed, 100 kg MIBK is added to stage 1 and 75 kg MIBK is added to stage 2. Calculate the flow rates and compositions of all named streams.



Raffinate 2: 43.1 kg total, 93.1% water, 5.3% acetone

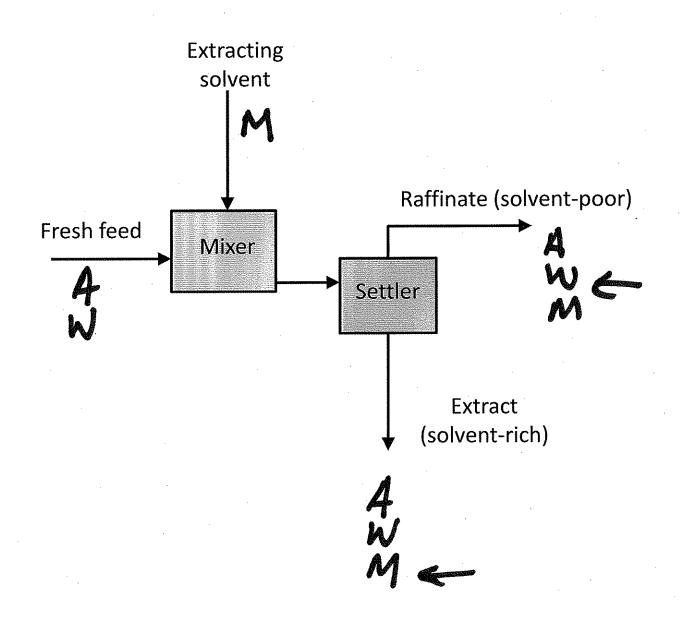
3

FR Example 4.4-2 (partial): The two-stage extraction process shown below is used to separate a 50/50 wt% mixture of acetone and water. The extraction solvent is methyl isobutyl ketone (MIBK). For every 100 kg of fresh feed, 100 kg MIBK is added to stage 1 and 75 kg MIBK is added to stage 2. Calculate the flow rates and compositions of all named streams.





Liquid-Liquid Extraction



75 K M 100ks M Raffinak Z 100 kg 43.1 ks total Fresh Fud KORLI BW 5045 A 2.2843 kg A 50 kg W 0.6896 kg M , Q, ky total = 231.900 kg W = 9.8739 distillation Q ks A = 47.7157 column Q, 15 M= 174.3104

Overall MASS Balance 100+100+75 = 43.1+ Q,

WATER

ACETONE

MIBK



PART 2: Inside Balances Choose the mixing point, where We know the most.

Ronau:

3867935 = 145.1065 Os Is total Qb ks both Extract 1 Exhete MIKING 27.5% A 9.0% A 0.295 Q ESA 0.09 Q6 65 A 231.9 ks ptal 9.8739 by W 47.7157 S A

174.3104 & M

MIXING POINT MASS BAL OVERALL



Q. + Q. = 23.9 kg QL = 231.9-Q 0.45 Qc + 0.09 QL = 47.7157 0.275 95 - 0.09 (231.9-05) = 47.7157 0.275 Q + 20.8710 - 0.09 Q = 47.7157 0.1850 = 26.8947 Cls = 145.1065 ks

867935 19

STAGE 2 BALANCES (rednaw)



75 kg M =54.8935 Qkshell Rethret Z Rathmaki B.I Es total 40.1261 kg hs 2.2 848 kg A 0.6896 kg M 86.7935 B HAL 2.6038 kg M 7.8114 ks A 76.3783 M

OVERALL MASS

Q + 75 = 43.1 + 86.7935

Q= 51. 8935 65

water bac

Q: = 40126/ 4 26038 = (42.7299 kg = Q;

ACETONE SAZ

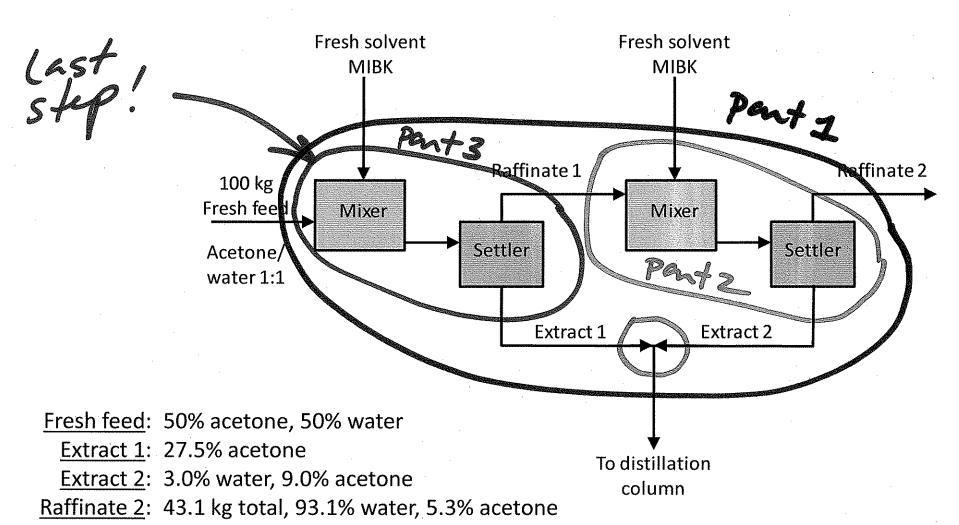
On = 2.2843 + 7.8114 = 10.0957 by = Qg

MIBK BA

 $Q_{10} + 75 = 0.6896 + 76.3783$ $Q_{10} = 2.0679 kg$



FR Example 4.4-2 (partial): The two-stage extraction process shown below is used to separate a 50/50 wt% mixture of acetone and water. The extraction solvent is methyl isobutyl ketone (MIBK). For every 100 kg of fresh feed, 100 kg MIBK is added to stage 1 and 75 kg MIBK is added to stage 2. Calculate the flow rates and compositions of all named streams.



STAGE 1 100 kg M ndraw: Rafforde/ looks btd 54.8935 to total 42.7299 Kg W 10.0957 to A 2. 0679 kg M 50Ks W Extrect 1

145.1065 to fotal 39.9043 ks A Qn ks W

Q₁, 5 W

STAGEI OVERALL MASS BAL (chek) 100 + 100 = SV. 8935 H/45.1065 ACETONE BAL (chede) 50 = 10.0957 + 39.9043 WATER BAL 50 kg = 42.7299 + Q11 Kemeining: Q11 = 7.2701 KS - 519 F125=3 - Mass 2

 $\frac{M16284}{100} = 2.0679 + Q_{12}$ $Q_{12} = 97.9321 \text{ (s)}$

calculations