

# Requests for today?

HW Prob

- 
- 7 sketches -  $k$  vs  $h$
  - 12 micro E bal
  - 14 fluids data correlations
  - heat " "
  - 15 nat'l conv + radiation
  - 21

Ex 2019  
#4

- ✓ 17
- ✓ 18
- ✓ 11
- ✓ 13

MEB

Q from  $\underline{V}$   
E from  $\underline{V}$

Temp micro E bal  
given  $T(r)$   $q_{r=}$ ?

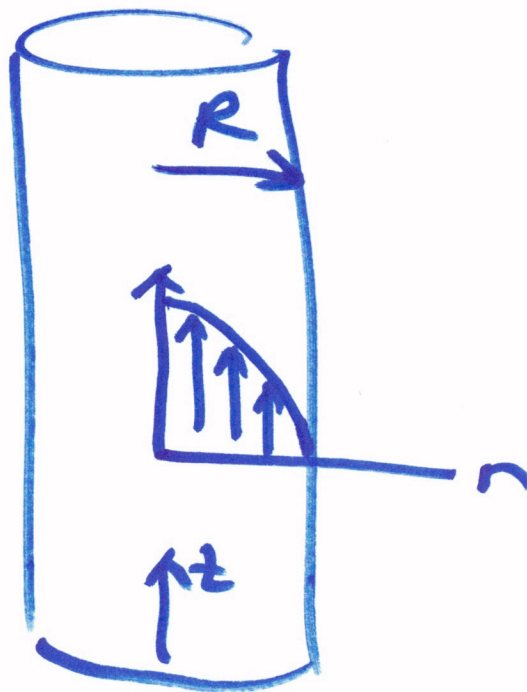
HW1 prob 17

book:  
UFM 6.21

15 Jan 2021 (1)

$$Q = \iint_S (\hat{n} \cdot \underline{v}) v_z \, dS$$

$\underbrace{dS}_{r dr d\theta}$



$$S = \pi R^2$$

cross  
sectional  
area

$$Q = \int_0^R \int_0^{2\pi} v_z r dr d\theta$$

$$\int_0^{2\pi} d\theta = \theta \Big|_0^{2\pi} = 2\pi$$

(2)

$$\frac{Q}{2\pi} = \int_0^R 12.0 \left( 1 - \frac{r^2}{\underbrace{0.012^2}_R} \right) r \, dr$$

$$\frac{Q}{(2\pi)(12.0)} = \int_0^R \left( r - \frac{r^3}{R^2} \right) dr$$

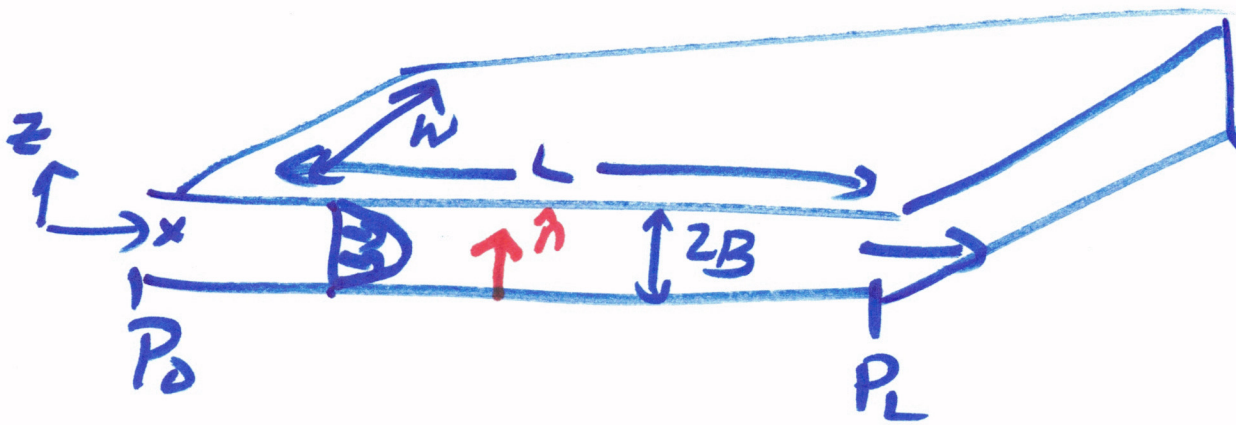
$$\left( \frac{r^2}{2} - \left( \frac{1}{R^2} \right) \frac{r^4}{4} \right) \Big|_0^R$$

$$\frac{R^2}{2} - \frac{R^2}{4} = \frac{R^2}{4}$$

$$Q = \frac{R^2}{4} (2\pi)(12.0) //$$

1.18

(3)



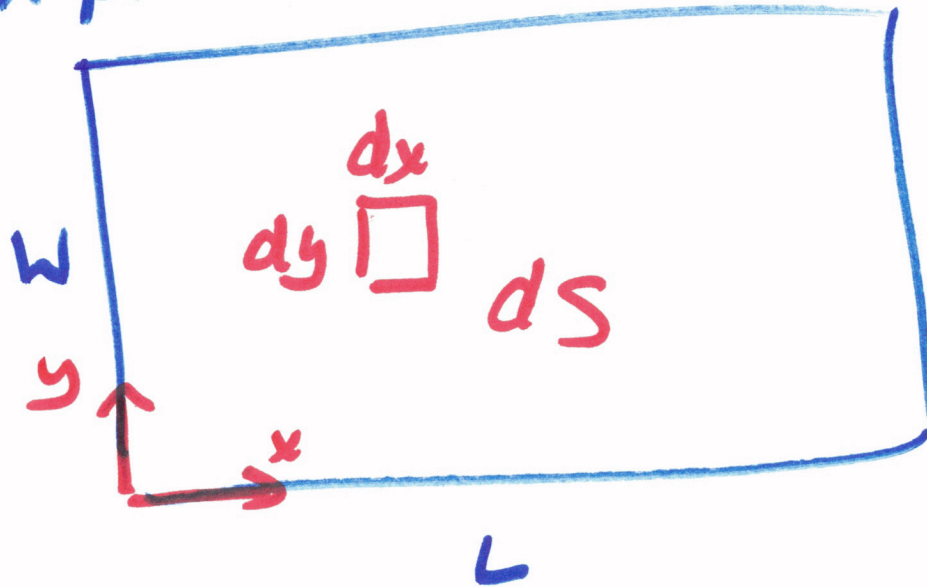
$P = cx$  pressure distribution  
 $-B < z < B$

$$\underline{F} = \int_{S_0}^w \left( \hat{n} \cdot \underline{\hat{T}} \right) \underbrace{dx dy}_{dS} \text{ at the surface } z = -B$$

$$\hat{n} = \begin{pmatrix} n_x \\ n_y \\ n_z \end{pmatrix}_{xyz} = \begin{pmatrix} 0 \\ 0 \\ 1 \end{pmatrix}_{xyz}$$

normal to bottom plate, "wet" side

bottom plate ( $z=B$ )



$$-\left(\frac{2\mu A}{B^2}\right)z$$

$$0 \leq x \leq L$$

$$0 \leq y \leq W$$

$$\hat{n} \cdot \underline{\underline{\tilde{\Pi}}} = \begin{pmatrix} 0 & 0 & 1 \end{pmatrix} \begin{pmatrix} -P & 0 & B\alpha \\ 0 & -P & 0 \\ B\alpha & 0 & -P \end{pmatrix}$$

$$= (B\alpha \ 0 \ -P)_{x,y,z}$$

(5)

$$\underline{F} = \int_0^w \int_0^L \begin{pmatrix} B\alpha \\ 0 \\ -p \end{pmatrix}_{xyz} dx dy$$

$$F_x = \int_0^w \int_0^L \overset{\text{constant}}{B\alpha} dx dy$$

$$\begin{aligned} B\alpha \times \frac{L}{0} &= B\alpha L \\ \int_0^w B\alpha L dy &= B\alpha L \cdot \frac{y}{0} \Big|_0^w \\ &= B\alpha L w \end{aligned}$$

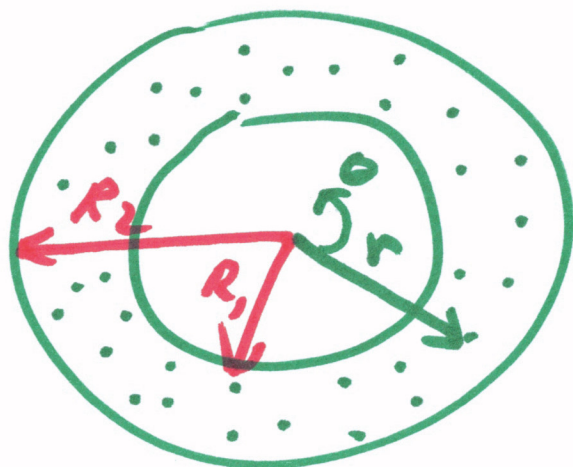
$$F_x = \cancel{B} L W \left( \frac{2 \mu A}{\cancel{B}^2} \right)$$

$$F_x = \frac{2 \mu A L W}{B}$$

⑥

1.11 (HW1)

7



$$R_1 \leq r \leq R_2$$

$$0 \leq \theta \leq 2\pi$$

$$r = R_1 \quad T = T_1$$

$$r = R_2 \quad T = T_2$$

What is  $T(r)$ ?



The **Equation of Energy** for systems with **constant k**

Microscopic energy balance, constant thermal conductivity; Gibbs notation

$$\rho \hat{c}_p \left( \frac{\partial T}{\partial t} + \underline{v} \cdot \nabla T \right) = k \nabla^2 T + S_e$$

Microscopic energy balance, constant thermal conductivity; Cartesian coordinates

$$\rho \hat{c}_p \left( \frac{\partial T}{\partial t} + v_x \frac{\partial T}{\partial x} + v_y \frac{\partial T}{\partial y} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + S_e$$

Symmetry

Microscopic energy balance, constant thermal conductivity; cylindrical coordinates

$$\rho \hat{c}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right) + S_e$$

Microscopic energy balance, constant thermal conductivity; spherical coordinates

$$\rho \hat{c}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi} \right) = k \left( \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} \right) + S_e$$

no rxn  
no elec  
current

v=0 pipe is solid

$$r \frac{0}{k} = \frac{k}{k} \frac{d}{dr} \left( r \frac{dT}{dr} \right)$$

$$0 = \frac{d}{dr} \left( r \frac{dT}{dr} \right)$$

≡ Φ

Reference: F. A. Morrison, "Web Appendix to An Introduction to Fluid Mechanics," Cambridge University Press, New York, 2013 ([pages.mtu.edu/~fmorriso/cm310/IFMWebAppendixDMicroEBalanceMorrison.pdf](http://pages.mtu.edu/~fmorriso/cm310/IFMWebAppendixDMicroEBalanceMorrison.pdf)). This worksheet is on the web at [pages.mtu.edu/~fmorriso/cm310/energy.pdf](http://pages.mtu.edu/~fmorriso/cm310/energy.pdf).

(8)

$$\frac{d\Phi}{dr} = 0$$

$$r \frac{dT}{dr} = \Phi = 0 + C_1 = C_1$$

$$\frac{dT}{dr} = C_1 \left( \frac{1}{r} \right)$$

$$T = C_1 \ln r + C_2$$

BC:  $r = R_1 \quad T = T_1$   $\left\{ \begin{array}{l} T_1 = C_1 \ln R_1 + C_2 \\ T_2 = C_1 \ln R_2 + C_2 \end{array} \right.$   
 $r = R_2 \quad T = T_2$

2 eqns, 2 unknowns

$\ln R_1/R_2$

①

subtract:

$$T_1 - T_2 = c_1 (\ln R_1 - \ln R_2)$$

$$c_1 = \frac{(T_1 - T_2)}{\ln \frac{R_1}{R_2}}$$

substitute:

$$T_1 = \left( \frac{T_1 - T_2}{\ln \frac{R_1}{R_2}} \right) \ln R_1 + c_2$$

(or could substitute into the other eqn)  
bc

Answer:

$$T = \left( \frac{T_1 - T_2}{\ln \frac{R_1}{R_2}} \right) \ln r + \overbrace{T_1 - \left( \frac{T_1 - T_2}{\ln \frac{R_1}{R_2}} \right) \ln R_1}^{c_2}$$

(10)

$$T - T_1 = \left( \frac{T_1 - T_2}{\ln R_1} \right) (\ln r - \ln R_1)$$

$$\left( \frac{T - T_1}{T_1 - T_2} \right) = \frac{\ln \frac{r}{R_1}}{\ln \frac{R_1}{R_2}}$$

1.13 (HW1) Calc radial flux  
Expand  $T(r)$  algebraically:

(11)

$$T = T_{b2} + \left( \frac{T_{b1} - T_{b2}}{\frac{k}{h_2 R_2} + \ln \frac{R_2}{R_1} + \frac{k}{h_1 R_1}} \right) \ln \frac{R_2}{r} + \left( \frac{k}{h_2 R_2} \right) \beta$$

$$T = T_{b2} + \alpha \ln \frac{R_2}{r} + \beta$$

$$= T_{b2} + \alpha (\ln R_2 - \ln r) + \beta$$

$$= \underbrace{(T_{b2} + \alpha \ln R_2 + \beta)}_{\delta} - \alpha \ln r$$

$$T = \delta - \alpha \ln r$$

$$\frac{q_r}{A} = -k \left( \frac{dT}{dr} \right) \quad \text{from above} \quad \text{Fourier's Law}$$

(12)

$$= -k \left( -\alpha \frac{1}{r} \right)$$

$$= \frac{k\alpha}{r} = \boxed{ k \left( \frac{T_{b1} - T_{b2}}{\frac{k}{h_2 R_2} + \ln \frac{R_2}{R_1} + \frac{k}{h_1 R_1}} \right) \frac{L}{r} = \frac{q_r}{A} }$$

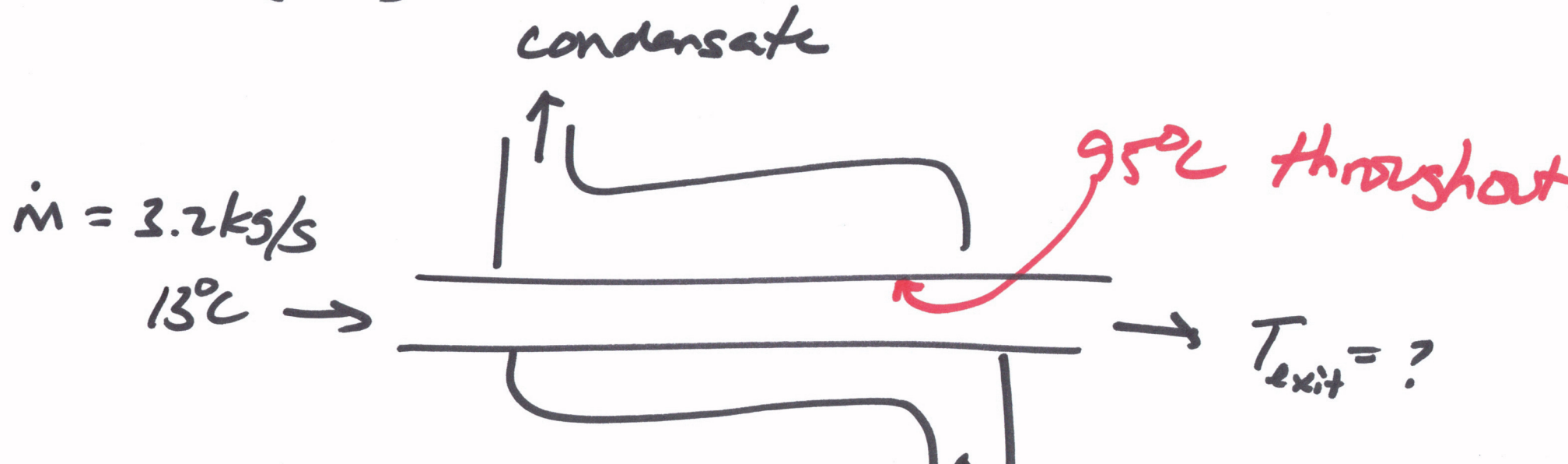
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STUDENT HOURS  
(following class)

Discussed HW1  
prob 15

1.15 (HW1)

OH 15 Jan 2021 ①



turbulent  
Sieder-Tate

$$\frac{\rho \check{V} D}{\mu}$$

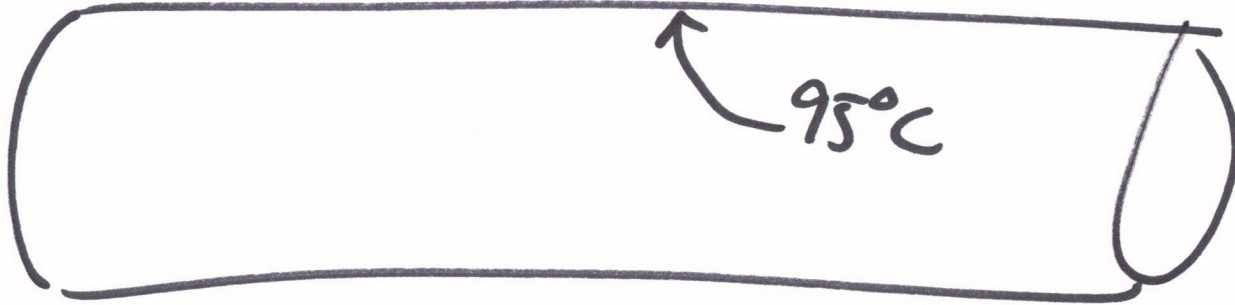
$$\frac{h_{lm} D}{k} = 0.027 Re^{0.8} Pr^{\frac{1}{3}} \left( \frac{\mu_b}{\mu_w} \right)^{0.14}$$

$$\dot{q}_{lm} = h_{lm} A \Delta T_{lm}$$

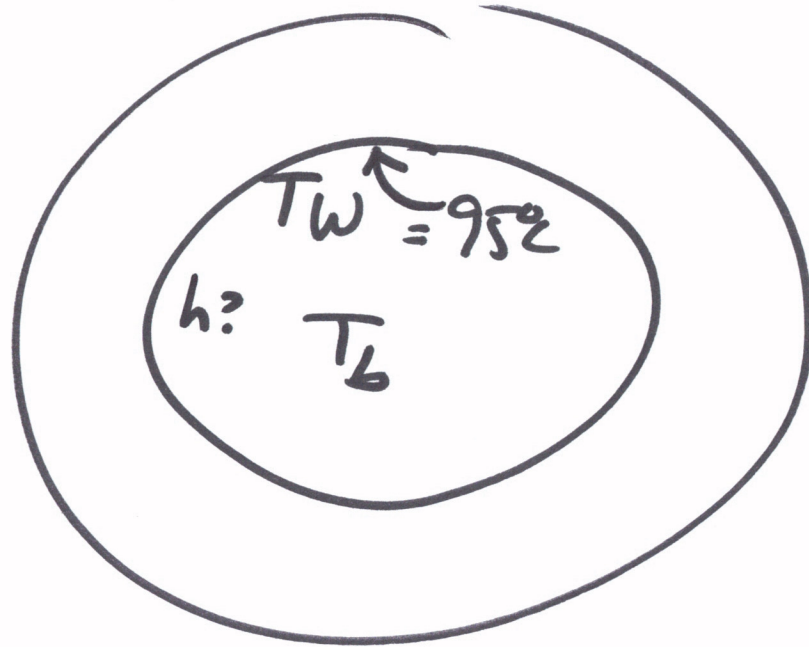
for h<sub>lm</sub> use  
Sieder-Tate  
equation



2



obtain  $h$   
from  
data  
correlations

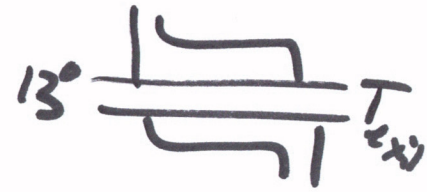


... (a)

$$h = 5300 \frac{W}{m^2K}$$

b) What is exit temperature?

PART OF SEIDER-TATE:



$$\dot{q}_{lm} = h_{lm} (\pi D L) \Delta T_{lm}$$

$$\Delta T_{lm} = \frac{(95 - 13) - (95 - T_{exit})}{\ln\left(\frac{95 - 13}{95 - T_{exit}}\right)}$$

equating; solve for T<sub>exit</sub>

MACRO E BAL INSIDE:

$$\cancel{\Delta E_p} + \cancel{\Delta E_k} + \Delta H = Q_{in} + \cancel{W_{s, on}}$$

$$\dot{q}_{lm} = \dot{Q}_{in} = \Delta H = \dot{m} \dot{c}_p (T_{exit} - 13^\circ C)$$