

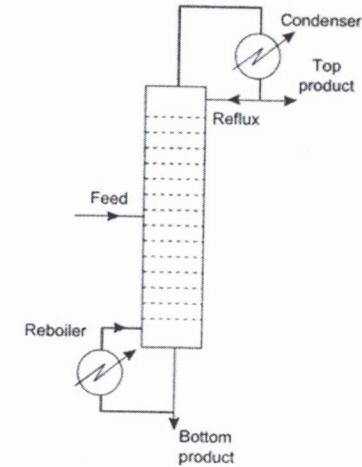
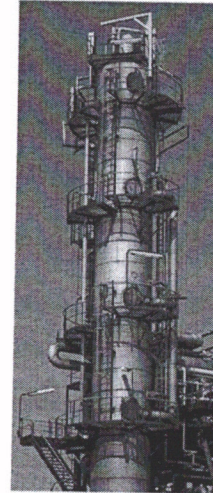


Mass transfer in Distillation

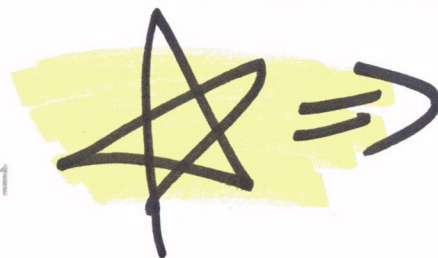
Example 4: Mass transfer in distillation

Equimolar Counter Diffusion

Example: Distillation



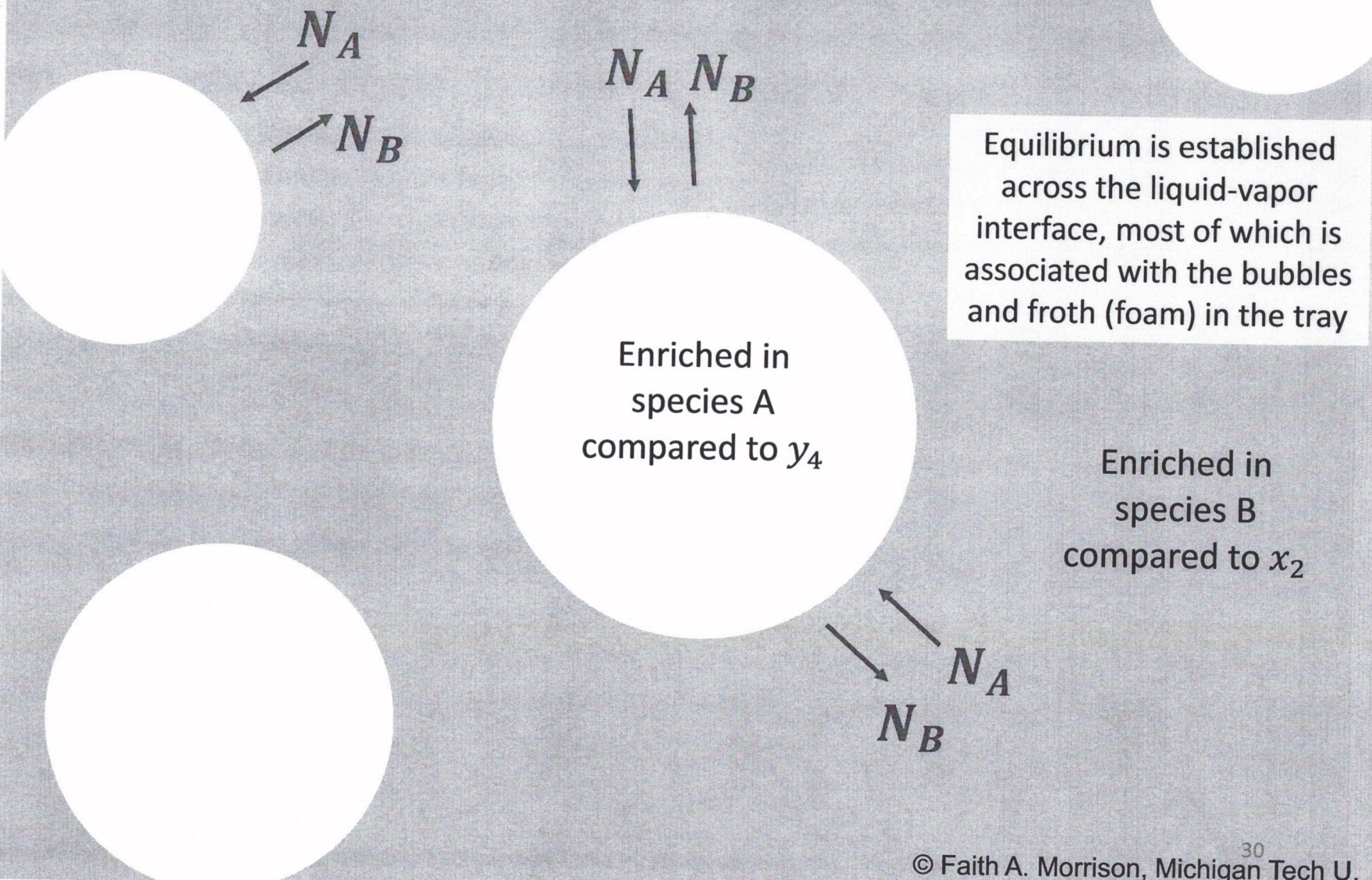
A distillation column is separating two components A and B at steady state. In the vapor phase of each equilibrium stage the two components are moving in **equimolar counter diffusion**. What are the molar fluxes of A and B in the vapor phase? What is the concentration distribution in the region of the equimolar counter diffusion?



MICROSCOPIC SPECIES A MASS BAL!

1.1

Equilibrium Stage

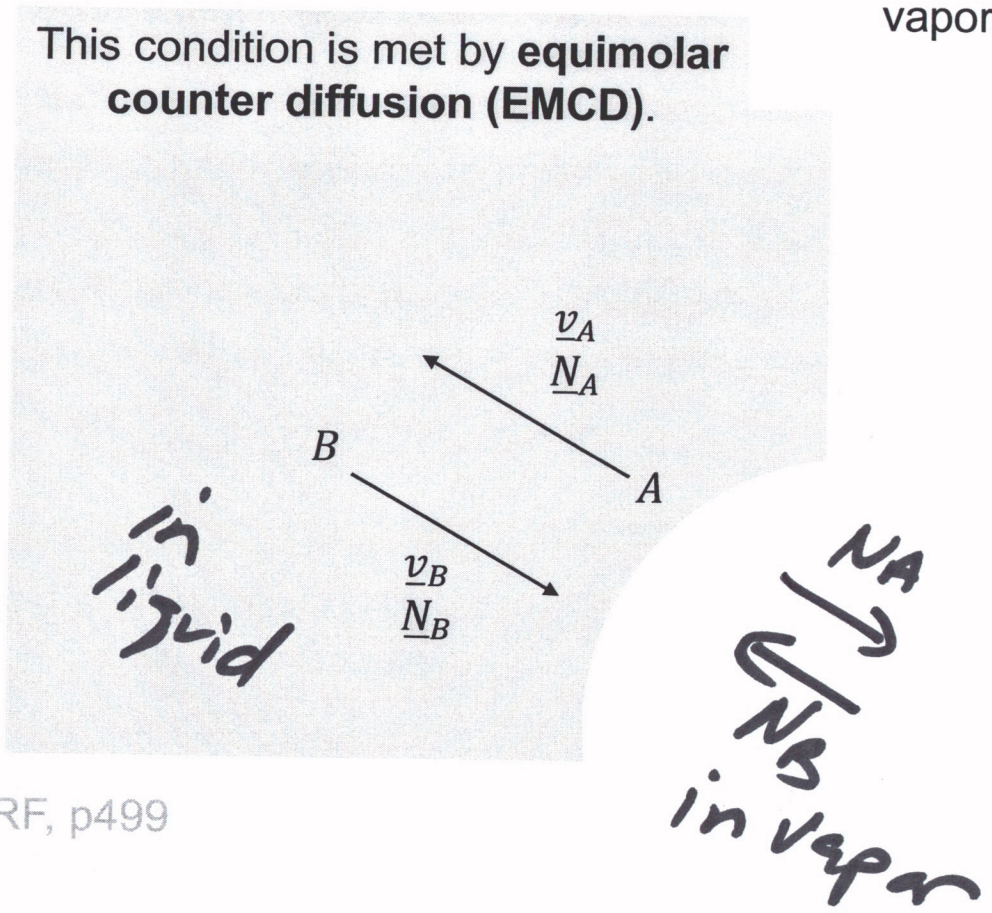


A Picture of Mass Transfer in Distillation

The molar flow rates throughout the enriching (L, V) and stripping (\bar{L}, \bar{V}) sections are constant if:

Every time a mole of vapor is condensed, a mole of liquid is vaporized (**Constant Molal Overflow**)

This condition is met by **equimolar counter diffusion (EMCD)**.



$$v_A = -v_B$$

$$N_A = -N_B$$

Note:

$$N_A + N_B = cv^*$$

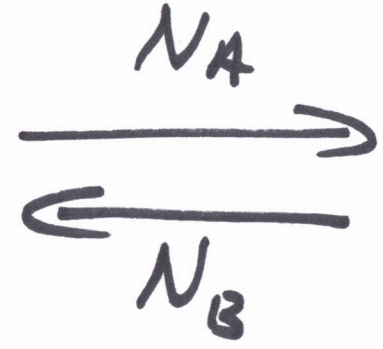
$$\Rightarrow v^* = 0$$

Equimolar counter diffusion

EMCD:

$$\underline{N}_A = -\underline{N}_B$$

$$\underline{N}_A + \underline{N}_B = 0$$



What is \underline{N}_A ?

$$z = z_1$$

$$x_A = x_{A1}$$

What is x_A ?

$$z = z_2$$

$$x_A = x_{A2}$$

$$\underline{N}_A = \begin{pmatrix} N_{Ax} \\ N_{Ay} \\ N_{Az} \end{pmatrix}_{x,y,z} = \begin{pmatrix} 0 \\ 0 \\ N_{Az} \end{pmatrix}_{x,y,z}$$

The Equation of Species Mass Balance in Terms of Combined

Molar quantities in Cartesian, cylindrical, and spherical coordinates for binary mixtures of A and B.

The general case, where the combined molar flux with respect to molar velocity (\underline{N}_A), is given on page 1.

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STEP 1

In terms of total molar flux, \underline{N}_A

Microscopic species mass balance, in terms of molar flux; Gibbs notation

$$\frac{\partial c_A}{\partial t} = -\nabla \cdot \underline{N}_A + R_A$$

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Microscopic species mass balance, in terms of combined molar flux; Cartesian coordinates

$$\frac{\partial c_A}{\partial t} = -\left(\frac{\partial N_{A,x}}{\partial x} + \frac{\partial N_{A,y}}{\partial y} + \frac{\partial N_{A,z}}{\partial z}\right) + R_A$$

Microscopic species mass balance, in terms of combined molar flux; cylindrical coordinates

$$\frac{\partial c_A}{\partial t} = -\left(\frac{1}{r} \frac{\partial(rN_{A,r})}{\partial r} + \frac{1}{r} \frac{\partial N_{A,\theta}}{\partial \theta} + \frac{\partial N_{A,z}}{\partial z}\right) + R_A$$

Microscopic species mass balance, in terms of combined molar flux; spherical coordinates

$$\frac{\partial c_A}{\partial t} = -\left(\frac{1}{r^2} \frac{\partial(r^2 N_{A,r})}{\partial r} + \frac{1}{r \sin \theta} \frac{\partial(N_{A,\theta} \sin \theta)}{\partial \theta} + \frac{1}{r \sin \theta} \frac{\partial N_{A,\phi}}{\partial \phi}\right) + R_A$$

Steps 1, 2, 3
no homogeneous

Fick's law of diffusion, Gibbs notation: $\underline{N}_A = x_A(\underline{N}_A + \underline{N}_B) - cD_{AB}\nabla x_A$

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$$= c_A \underline{v}^* - cD_{AB}\nabla x_A$$

STEP 2

Fick's law of diffusion, Cartesian coordinates:

$$\begin{pmatrix} N_{A,x} \\ N_{A,y} \\ N_{A,z} \end{pmatrix}_{xyz} = \begin{pmatrix} x_A(N_{A,x} + N_{B,x}) - cD_{AB} \frac{\partial x_A}{\partial x} \\ x_A(N_{A,y} + N_{B,y}) - cD_{AB} \frac{\partial x_A}{\partial y} \\ x_A(N_{A,z} + N_{B,z}) - cD_{AB} \frac{\partial x_A}{\partial z} \end{pmatrix}_{xyz}$$

Fick's law of diffusion, cylindrical coordinates:

$$\begin{pmatrix} N_{A,r} \\ N_{A,\theta} \\ N_{A,z} \end{pmatrix}_{r\theta z} = \begin{pmatrix} x_A(N_{A,r} + N_{B,r}) - cD_{AB} \frac{\partial x_A}{\partial r} \\ x_A(N_{A,\theta} + N_{B,\theta}) - \frac{cD_{AB}}{r} \frac{\partial x_A}{\partial \theta} \\ x_A(N_{A,z} + N_{B,z}) - cD_{AB} \frac{\partial x_A}{\partial z} \end{pmatrix}_{r\theta z}$$

Fick's law of diffusion, spherical coordinates:

$$\begin{pmatrix} N_{A,r} \\ N_{A,\theta} \\ N_{A,\phi} \end{pmatrix}_{r\theta\phi} = \begin{pmatrix} x_A(N_{A,r} + N_{B,r}) - cD_{AB} \frac{\partial x_A}{\partial r} \\ x_A(N_{A,\theta} + N_{B,\theta}) - \frac{cD_{AB}}{r} \frac{\partial x_A}{\partial \theta} \\ x_A(N_{A,\phi} + N_{B,\phi}) - \frac{cD_{AB}}{r \sin \theta} \frac{\partial x_A}{\partial \phi} \end{pmatrix}_{r\theta\phi}$$

MICRO SPECIES A MASS BAL:

(9)

$$\frac{dN_{A_2}}{dz} = 0$$

$$N_{A_2} = C_1$$

Fick's LAW of Diffusion

$$C_1 = N_{A_2} = -C D_{AB} \frac{dx_A}{dz} \quad (\text{from sheet})$$

constant \nearrow \nearrow constant \nearrow ?

Is c constant?

(5)

GAS PHASE (assume ideal)

$$PV = nRT$$

$$c = \frac{P}{RT} = \frac{n}{V} = \frac{\text{moles mix}}{\text{Volume mix}}$$

\Rightarrow constant!

Integrate:

$$\left(-\frac{q}{cD_{AB}} \right) = \frac{dx_A}{dz}$$

SOLVE,
Apply BC
calc c_1, c_2 //



Example 4: Mass transfer in distillation

A distillation column is separating two components A and B at steady state. In the vapor phase of each equilibrium stage the two components are moving in equimolar counter diffusion. What are the molar fluxes of A and B in the vapor phase? What is the concentration distribution in the region of the equimolar counter diffusion?



Answers:

$$N_{Az} = \frac{P_{A1} - P_{A2}}{(z_2 - z_1)} \left(\frac{D_{AB}}{RT} \right)$$

(constant flux proportional to D_{AB})

$$\frac{x_A - x_{A1}}{x_{A1} - x_{A2}} = \frac{z - z_1}{z_1 - z_2}$$

(linear concentration profile)

$$x_A = \left(\frac{x_{A1} - x_{A2}}{z_1 - z_2} \right) z - \frac{z_1(x_{A1} - x_{A2})}{z_1 - z_2} + x_{A1}$$