



## Requests for today?

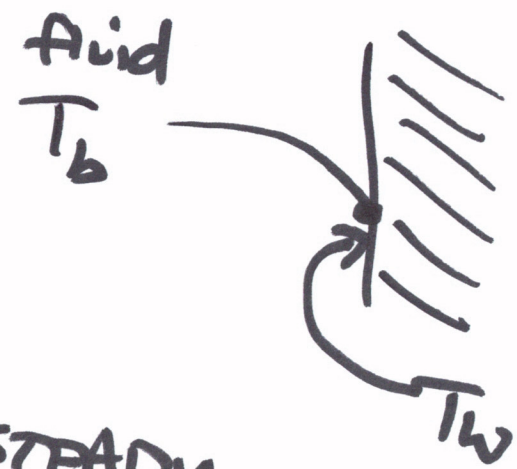
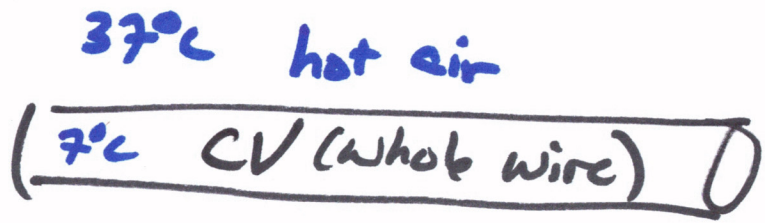
✓. HW 2.7

✓. HW 2.3

✓. HW 2.14 (separate video)

2.7

$$\left| \frac{q}{A} \right| = h \left| T_b - T_w \right|$$



SOLN: MACRO E BAL UNSTEADY

$$\frac{d}{dt} ( \underbrace{U_{sys}} + \cancel{E_k} + \cancel{E_p} ) = \cancel{-\Delta H} - \cancel{\Delta E_k} - \cancel{\Delta E_p} + \underbrace{Q_{in}} + \cancel{W_{s,in}}$$

neglect  $\dot{m} = 0$  no shaft

Internal energy:

- T-change
- phase-change
- chemical composition change

2

$$\frac{dU_{sys}}{dt} = Q_{in}$$

$$\rho V c_p \frac{dT}{dt} = h A (T_b - T_{wire})$$

mass  
of  
wire

$$A = \pi D L$$

$\boxed{\text{Volume}} \rightarrow \frac{\pi D^2}{4} V = \frac{\pi D^2 L}{4}$

$$\rho \frac{\pi D^2 L}{4} c_p \frac{dT}{dt} = h \pi D L (T_b - T_{wire})$$

$$\frac{dT}{dt} = \frac{h 4}{\rho c_p D} (T_b - T_{wire})$$

$$\frac{dT}{dt} = \tilde{\delta} (T_b - T)$$

$$(-1) \int \frac{-dT}{(T_b - T)} = \int \tilde{\delta} t$$

$$-\ln(T_b - T) = \tilde{\delta} t + C_1$$

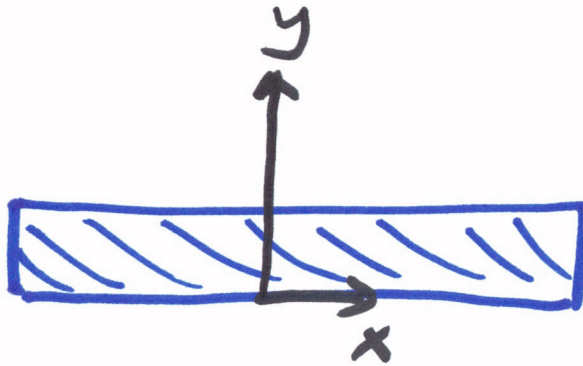
$$\text{IC: } t=0 \quad T=7^\circ\text{C} \Rightarrow C_1$$

ANSWER QUESTION:

$$t=30 \quad T=24^\circ\text{C} \quad (t, T) = (30, 24^\circ\text{C}) \\ \Rightarrow h. //$$

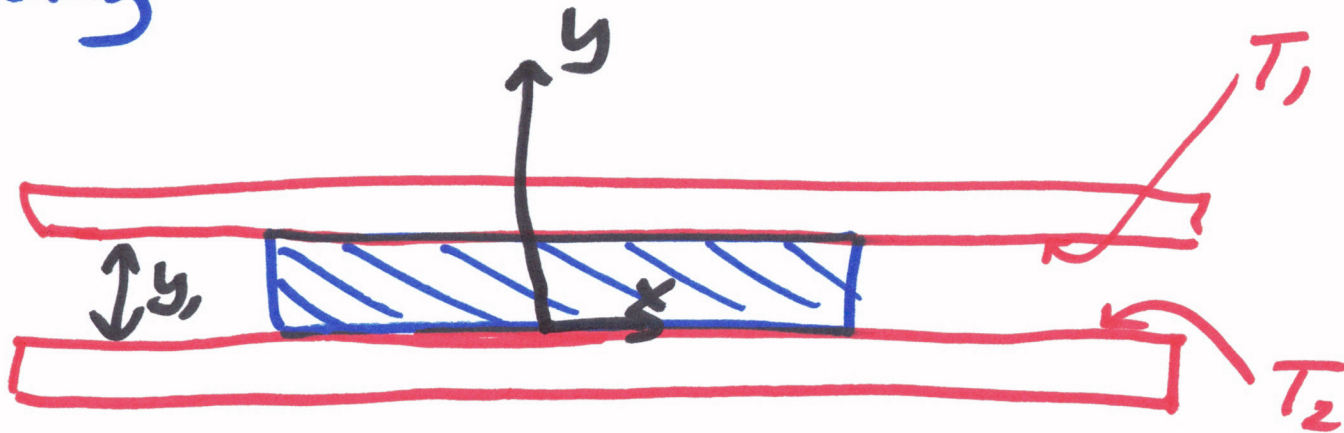
2.3 Develop  
model:

$$t=0$$
$$T = T_0$$



1D heat xfer  
in y dir  
 $T(y,$

"Suddenly"



$$y=0 \quad T = T_2$$
$$y=y_1 \quad T = T_1$$



# The Equation of Energy for systems with constant $k$

Microscopic energy balance, constant thermal conductivity; Gibbs notation

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + \underline{v} \cdot \nabla T \right) = k \nabla^2 T + S_e$$

Microscopic energy balance, constant thermal conductivity; Cartesian coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_x \frac{\partial T}{\partial x} + v_y \frac{\partial T}{\partial y} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + S_e$$

Microscopic energy balance, constant thermal conductivity; cylindrical coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right) + S_e$$

Microscopic energy balance, constant thermal conductivity; spherical coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi} \right) = k \left( \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} \right) + S_e$$

$v=0$

no current  
no rxn

$$\frac{\partial T}{\partial t} = \frac{k}{\rho \hat{C}_p} \frac{\partial^2 T}{\partial y^2}$$

BC:  $y=0 \quad T=T_2$   
 $y=y_1 \quad T=T_1$   
IC:  $t=0 \quad T=T_0$

determining this + the sketch is what is meant by "modeling" the plan.

Reference: F. A. Morrison, "Web Appendix to An Introduction to Fluid Mechanics," Cambridge University Press, New York, 2013 ([pages.mtu.edu/~fmorriso/cm310/IFMWebAppendixDMicroEBalanceMorrison.pdf](http://pages.mtu.edu/~fmorriso/cm310/IFMWebAppendixDMicroEBalanceMorrison.pdf)). This worksheet is on the web at [pages.mtu.edu/~fmorriso/cm310/energy.pdf](http://pages.mtu.edu/~fmorriso/cm310/energy.pdf).

(Separate video)

(6)

14. A brass sphere (diameter = 2.54 cm) initially at  $24^{\circ}\text{C}$  is suddenly immersed in vigorously stirred water ( $85^{\circ}\text{C}$ ). After 5.0 seconds the center of the sphere is observed to be ( $72^{\circ}\text{C}$ ). How long will it take the center of the sphere to reach  $T = 83.8^{\circ}\text{C}$ ?

$$T(r, t) = T(0, t)$$

Since it's a question about the temp profile, it's a microscopic energy bal plan.

(Slush + burn)

(Check if it's Heisler-compatible)



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Microscopic energy balance, constant thermal conductivity; cylindrical coordinates

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Microscopic energy balance, constant thermal conductivity; spherical coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi} \right) = k \left( \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} \right) + S_e$$

no abc current  
no rkn

$\underline{v} = 0$

$\theta, \phi$  symmetry

$$\frac{\partial T}{\partial t} = \frac{k}{\rho \hat{C}_p} \left( \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) \right)$$

IC:  $t < 0 \quad T = 24^\circ\text{C} \quad \forall r$   
 $= T_0$

BC:  $r = R$  Newton's Law of cooling

Reference: F. A. Morrison, "Web Appendix to An Introduction to Fluid Mechanics," Cambridge University Press, New York, 2013 ([pages.mtu.edu/~fmorriso/cm310/IEMWebAppendixDMicroEBalanceMorrison.pdf](http://pages.mtu.edu/~fmorriso/cm310/IEMWebAppendixDMicroEBalanceMorrison.pdf)). This worksheet is on the web at [pages.mtu.edu/~fmorriso/cm310/energy.pdf](http://pages.mtu.edu/~fmorriso/cm310/energy.pdf).

$r=0 \quad \frac{\partial T}{\partial r} = 0 \quad T_b = T_i = 85^\circ\text{C}$

yo, it's the Heisla plan



# RULES FOR HEISLER, Gurney-Lurie:



## 1D Unsteady Heat Transfer: Finite Bodies

### Finite 1D Unsteady Heat Transfer, $T = T(t, x)$ or $T = T(t, r)$

Uniform initial temperature  $T_0$ ; exposed to bulk temperature  $T_1$ ;  $h$  known

- Flat plate long, wide, thickness =  $2x_1$   $T = T(t, x)$   $Y = Y(X, n)$
- Cylinder long, radius =  $x_1$   $T = T(t, r)$   $Y = Y(X, n)$
- Sphere radius =  $x_1 = \frac{2.54}{2} \text{ cm}$   $T = T(t, r)$   $Y = Y(X, n)$

$$\text{Bi} = \frac{hD_{\text{char}}}{k} = \frac{hx_1}{k} = \frac{1}{m}$$

$$\text{Fo} = \frac{\alpha t}{x_1^2} = X$$

$$\frac{x}{x_1} = \frac{r}{x_1} = n$$

$$\frac{T_1 - T}{T_1 - T_0} = Y \quad \left( \frac{T - T_0}{T_1 - T_0} = 1 - Y \right)$$

**Note:**

$$D_{\text{char}} = x_1, \\ \text{NOT } V/A$$

$$\alpha = 3.28 \times 10^{-5} \frac{\text{m}^2}{\text{s}}$$

$$x_1 = 1.27 \times 10^{-2} \text{ m}$$

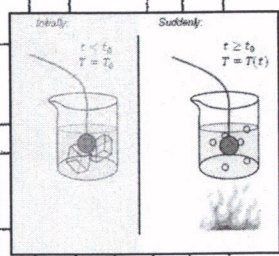
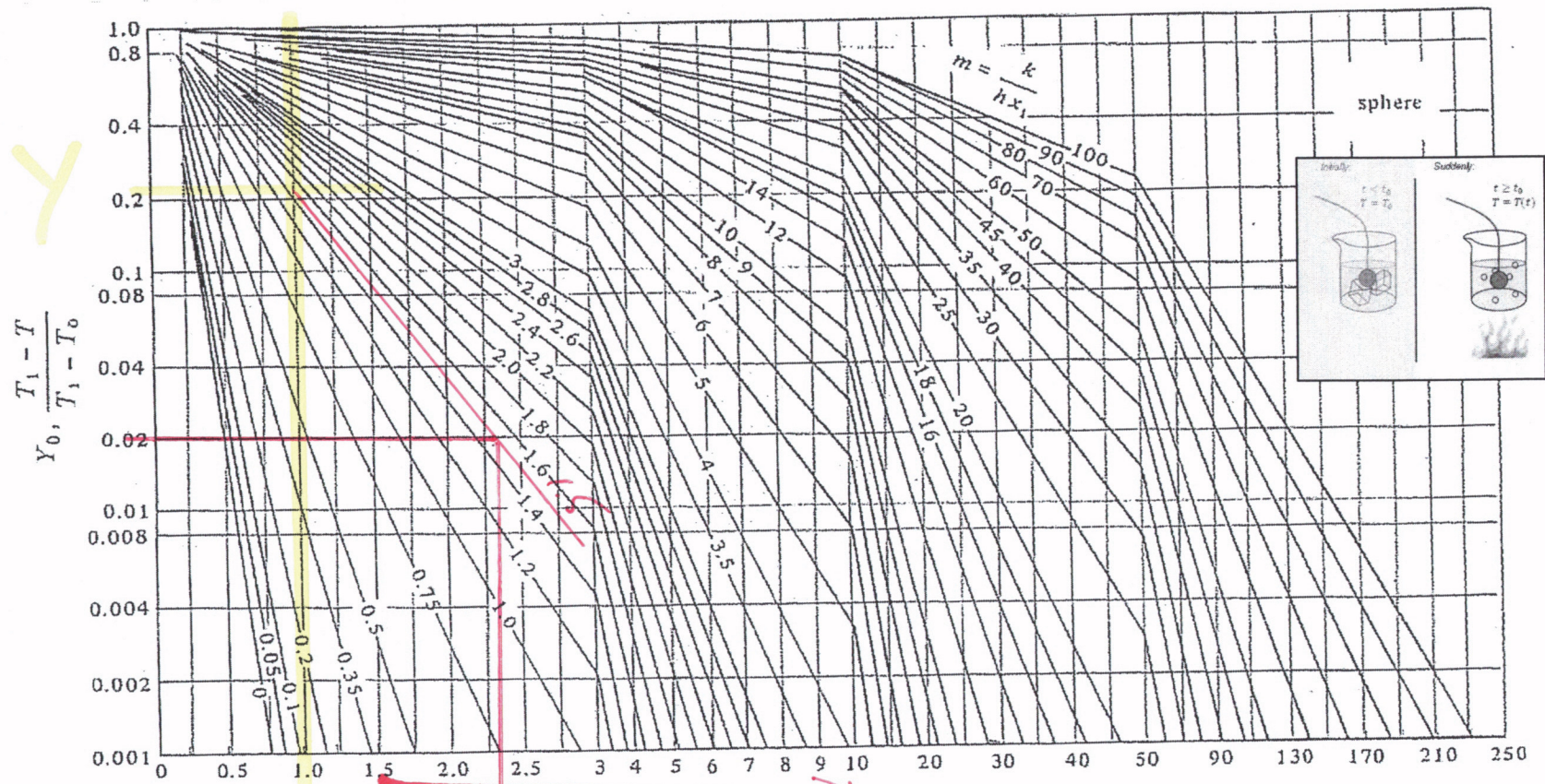
$$\text{Fo}(5\text{s})$$

$$= 1.02 \sim 1$$



# Heisler Chart for Unsteady State Heat Transfer to a Sphere

(Geankoplis; see also Wikipedia)



$F_0 = 2.3$   $t = 1 \text{ sec}$   $X = \frac{\alpha t}{x_1^2}$  **answer**

FIGURE 5.3-10. Chart for determining the temperature at the center of a sphere for unsteady-state heat conduction. [From H. P. Heisler, Trans. A.S.M.E., 69, 227 (1947). With permission.]

From Geankoplis, 4<sup>th</sup> edition, page 374

$\alpha = 3.28 \times 10^{-5} \text{ m}^2/\text{s}$   
 $R = x_1 = 1.27 \times 10^{-2} \text{ m}$

FIRST POINT: at  $Fo = 1 = \frac{\alpha t}{R^2}$   $85^\circ C = T_1 - T = 72$  (10)

$$\frac{85^\circ C - T}{85^\circ C - 24^\circ C} = 0.21$$

$85^\circ C$        $24^\circ C$

From Heisler:  $m = 1.5 = \frac{k}{hR}$

(we now know the m-line for the 2nd pt)

2nd pt: after t seconds  $T = 83.8$

$$Y = \frac{85 - 83.8}{85 - 24} = 0.02 \leftarrow \text{What is } Fo = \frac{\alpha t}{R^2}$$

for  $m = 1.5$ ?