

MOD 4 STUDY GUIDE #9

14 Apr 2024
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Explain linear driving force model
to an interface (k_x) + compare to
Fick's LAW

What is Fick's Law? } (p2)
What is LDF model? }

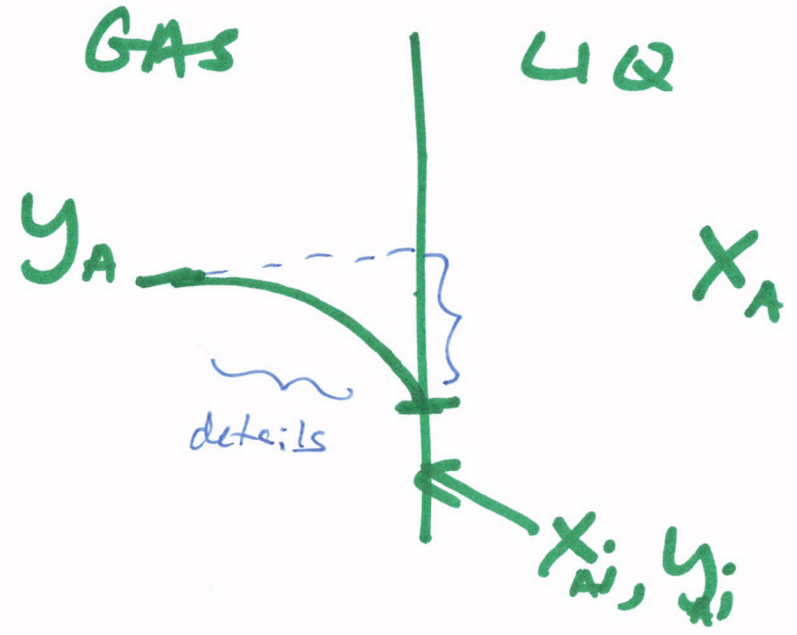
How are they used in } (p3)
mass x fu }

Compare + contrast } (p4)

Fick's Law

$$N_{A_z} \propto \frac{dx_A}{dz}$$

$$N_{A_z} \propto \frac{dy_A}{dz}$$



localized flux value or flux as function of position

LDF

$$(y_A - y_{Ai}) k_y = N_A$$

details are "LUMPED" together

↑
get from data correlations (scenario property)

Microscopic C.V.

micro spec A mole B-1
Fick's Law

$$\frac{\partial C_A}{\partial t} = -\nabla \cdot \underline{N}_A + R_A$$

$$N_A = x_A (N_A + N_B) - C D_{AB} \nabla x_A$$

MACROSCOPIC C.V.

MACRO spec A mole B-1

$$\frac{dM_A}{dt} = -\Delta \dot{M}_A - R_A V_{vol} - N_{AS}$$

S.A. mass xfr

LDF_{model}:

$$N_A = K \Delta C_d = K_y (y_A - y_A^*(x_A))$$

Compare + contrast:

at phase interface

Q

D_{AB}
(FICK'S
LAW)

k_y
(LDF)
model

gives detailed
 $N_A(z)$
has a func
of position

D_{AB} = material
parameter
(look up)

complex to do
in non-simple
scenarios

(usually)

MICRO C.V.

Lumped approach
(simplified
 $N_A \propto (y_A - y_{A,i})$)

k_y is a scenario
property

much more accessible
in non-simple scenarios
(but need data
correlations)

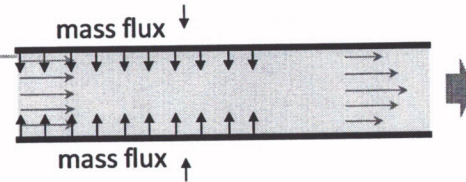
MACRO C.V.

$Sh(Re, Sc, \frac{L}{D})$

LEET VII MOD 4



Dimensional Analysis in Mass Transfer



Example 15

According to our **dimensional analysis** calculations, the dimensionless heat transfer coefficient should be found to be a function of three dimensionless groups:

Peclet number

$$Pe_m = ReSc = \frac{VD}{D_{AB}}$$

Schmidt number

$$Sc = \frac{\mu}{\rho D_{AB}}$$

$$Sh = Sh \left(Re, Sc, \frac{L}{D} \right)$$

Now, do the experiments.

$$Sh = \frac{k_c D}{D_{AB}}$$

*dimensionless
mass xfer coef*

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(compare w/ Nu)



Dimensionless Numbers

Dimensionless numbers from the **Equations of Change**

$$\text{Re} - \text{Reynolds} = \frac{\rho V D}{\mu} = \frac{V D}{\nu}$$

$$\text{Fr} - \text{Froude} = \frac{v^2}{g D}$$

$$\text{Pe} - \text{Péclet}_h = \text{RePr} = \frac{\hat{C}_p \rho V D}{k} = \frac{V D}{\alpha}$$

$$\text{Pe} - \text{Péclet}_m = \text{ReSc} = \frac{V D}{D_{AB}}$$

$$\text{Pr} - \text{Prandtl} = \frac{\hat{C}_p \mu}{k} = \frac{\nu}{\alpha}$$

$$\text{Sc} - \text{Schmidt} = \text{LePr} = \frac{\mu}{\rho D_{AB}} = \frac{\nu}{D_{AB}}$$

$$\text{Le} - \text{Lewis} = \frac{\alpha}{D_{AB}}$$

These numbers tell us about the **relative importance of the terms** they precede in the microscopic balances (*scenario properties*).

These numbers compare the **magnitudes of the diffusive transport coefficients** ν, α, D_{AB} (*material properties*).

Dimensional Analysis

These numbers are defined to help us build **transport data correlations** based on the fewest number of grouped (dimensionless) variables (*scenario property*).

Dimensionless numbers from the Engineering Quantities of Interest

momentum

Dimensionless Force on the Wall (Drag)

$$f = \frac{1}{\pi} \frac{D}{L} \frac{1}{\text{Re}} \int_0^{\frac{L}{D}} \int_0^{2\pi} \left. \left(\frac{\partial v_z^*}{\partial r^*} \right) \right|_{r^*=\frac{1}{2}} d\theta dz^*$$

f – Friction Factor
 $\frac{L}{D}$ – Aspect Ratio

$$f = \frac{\mathcal{F}_{drag}}{\left(\frac{1}{2} \rho V^2 \right) A_c}$$

energy

Newton's Law of Cooling

$$\text{Nu} = \frac{1}{2\pi L / D} \int_0^{\frac{L}{D}} \int_0^{2\pi} \left. \frac{\partial T^*}{\partial r^*} \right|_{r^*=\frac{1}{2}} dz^* d\theta$$

Nu – Nusselt
 $\frac{L}{D}$ – Aspect Ratio

$$\text{Nu} = \frac{hD}{k}$$

$$\text{St}_h = \frac{h}{\rho V \hat{C}_p} = \frac{\text{Nu}}{\text{RePr}}$$

mass xfer

Dimensionless Mass Transfer Coefficient

$$\text{Sh} = \frac{1}{2\pi L} \int_0^{\frac{L}{D}} \int_0^{2\pi} \left. \left(-\frac{\partial x_A^*}{\partial r^*} \right) \right|_{r^*=\frac{1}{2}} d\theta dz^*$$

Sh – Sherwood
 $\frac{L}{D}$ – Aspect Ratio

$$\text{Sh} = \frac{k_c D}{\mathcal{D}_{AB}}$$

$$\text{St}_m = \frac{k_c}{V} = \frac{\text{Sh}}{\text{ReSc}}$$

St – Stanton