## Study Guide for CM3120 Transport II Module 4 Diffusion and Mass Transfer II and Unit Operations Morrison Spring 2021

Test subjects in this course are cumulative. Anything on a study guide from a prior exam may be the subject of a current exam.

Exam 4 (the final exam) will cover, in addition to Exam 1-3 topics, the topics listed below.

## To do well on the test, you should be able to do the following:

Using classical mass-transfer solutions (Part II Equimolar counter diffusion; penetration model)

- 1. Explain resistance to mass transfer; indicate what chemical engineering processes affected by mass-transfer resistance
- 2. Explain the "constant molal overflow" assumption in distillation; identify the physics that makes this assumption plausible
- 3. Apply equimolar counter diffusion model to determine concentration distributions and mass transfer engineering quantities of interest
- 4. Apply the penetration model to determine concentration distributions and mass transfer engineering quantities of interest
- 5. Choose among appropriate "classic" mass-transfer models to evaluate the importance of mass transfer in an engineering scenario
- 6. Continue to demonstrate proficiency with module-3 and other prior study-guide objectives, including applying the mechanical energy balance
- 7. (optional) Apply pseudo-steady-state solution methods to species A mass transfer problems (macroscopic control volumes)

Linear driving force model for transfers at or across boundaries (film mass transfer coefficients,  $k_x$ ,  $k_c$ ,  $k_p$  and overall mass transfer coefficients  $K_L$ ,  $K_G$ )

- 8. Explain the role of chemical equilibrium in identifying the driving force for mass transfer
- 9. Explain the linear driving force model for mass transfer to an interface (employing film mass transfer coefficient  $k_x$ ) and compare it to Fick's law of diffusion
- 10. Explain the linear driving force model for mass transfer from one bulk phase to another (employing overall mass transfer coefficients  $K_L$ ,  $K_G$ ) and compare it to the heat exchanger design equation  $\dot{Q} = UA\Delta T_{lm}$
- 11. Calculate engineering quantities of interest with the macroscopic species A mass balance incorporating transfers at boundaries
- 12. Evaluate predictions of mass transfer coefficient from microscopic models of diffusion and mass transfer
- 13. Calculate liquid-side-units and gas-side-units overall mass transfer coefficients from associated film coefficients.

Macroscopic species A mass balance-steady and unsteady

- 14. List the contributions to the macroscopic species A mass balance on unit operations and indicate how each is typically evaluated
- 15. Explain how mass transfer is accounted for in the macroscopic species A mass balance
- 16. Simplify and solve the macroscopic species A mass balance for elementary unsteady scenarios such as evaporating liquids or dissolving solids
- 17. Simplify and solve the macroscopic species A mass balance for elementary steady scenarios such as in gas absorption

Dimensional analysis in mass transfer, conditions at the boundary (complex mass-transfer systems involving <u>bulk convection</u>)

- 18. Explain the purpose of dimensional analysis in mass-transfer engineering
- 19. Explain the meaning of *data correlation*; explain where and how we obtain mass transfer data correlations
- 20. List, define, and explain the use of at least three dimensionless numbers in mass transfer
- 21. List two examples of data correlations for Sherwood number Sh (give the equation, the name of the correlation if it has one, and identify the symbols, including the material it applies to). Indicate when the correlations apply
- 22. Identify pairs of unsteady state heat transfer and mass transfer problems that are governed by the same mathematics, including boundary conditions
- 23. Use heat-transfer results (for example, Heisler charts) to address answers to mass transfer questions
- 24. Explain the use of the analogy between heat and mass transfer to determine data correlations for Sherwood number Sh
- 25. Identify analogous Sh(Re,Sc) correlations from Nu(Re,Pr) heat-transfer correlations

Unit operations and devices (mass transfer dominated,  $K_L, K_G$ )

- 26. Carry out a McCabe-Thiele analysis to determine the number of equilibrium stages needed to carry out a separation
- 27. Explain the operating line in mass-transfer unit operations modeling; identify the physics that gives the operating line
- 28. Explain the equilibrium curve in mass-transfer unit operations modeling; identify the physics that gives the equilibrium curve
- 29. Compare and contrast the operation and modeling of staged distillation columns and continuous distillation columns
- 30. Define and explain the meaning and utility of NTU and HTU in mass-transfer unit operations modeling
- 31. Explain how mass-transfer issues affect the efficiency of a distillation column or a gas absorption column
- 32. Calculate NTU and HTU for a continuous distillation operation (size a continuous distillation column)
- 33. Calculate NTU and HTU for a gas absorption tower (size a gas absorption tower))
- 34. Apply macroscopic species A mass balances to unit operations to determine size-related parameters

Unit operations: Distillation (UO Worksheet)

- 35. Explain in one to three sentences the operating principle of a distillation column
- 36. List at least two actual engineering processes that employ distillation columns; one should be the most common
- 37. List three limitations of this unit operation

Unit operations: Gas absorption (UO Worksheet)

- 38. Explain in one to three sentences the operating principle of a gas absorption column
- 39. List at least two actual engineering processes that employ gas absorption columns; one should be the most common
- 40. List three limitations of this unit operation

Unit operations: Membrane separation (UO Worksheet)

- 41. Explain in one to three sentences the operating principle of membrane separation
- 42. List at least two actual engineering processes that employ membrane separation; one should be the most common
- 43. List three limitations of this unit operation

Unit operations: Liquid-Liquid Extraction (UO Worksheet)

- 44. Explain in one to three sentences the operating principle of a liquid-liquid extraction column
- 45. List at least two actual engineering processes that employ liquid-liquid extraction columns; one should be the most common
- 46. List three limitations of this unit operation

## Mass transfer troubleshooting

- 47. Compare and contrast steady and unsteady mass transfer scenarios
- 48. From among mass transfer tools (microscopic species A mass balance, macroscopic species A mass balance, linear driving force models) identify the method that may result in the missing desired quantity (amount of species A transferred, mass of species A flux, concentration field, etc.) for unsteady state mass transfer scenarios
- 49. List, in an order that works, steps for determining a quantity with the mass transfer tools at your disposal

## <u>References:</u>

- Christie J. Geankoplis, *Transport Processes and Unit Operations*, 4th Edition, Prentice Hall, New York (2003)
- *Perry's Handbook of Chemical Engineering*, 8<sup>th</sup> Edition (McGraw-Hill Professional, New York, 2007).
- Phillip C. Wankat, *Separation Process Engineering*, 4<sup>th</sup> edition, Prentice Hall, New York (2017)
- E. L. Cussler, Diffusion: Mass Transfer in Fluid Systems, 3rd Edition, Cambridge University Press, New York (2009).
- James R. Welty, Gregory L. Rorrer, and David G. Foster, *"Fundamentals of Momentum, Heat, and Mass Transfer,"* 6<sup>th</sup> edition (Wiley, New York, 2015).