CM3120 Transport/Unit Operations 2

Unsteady State Heat Transfer

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www.chem.mtu.edu/~fmorriso/cm3120/cm3120.html

 1

Heat Transfer: Steady vs. Unsteady

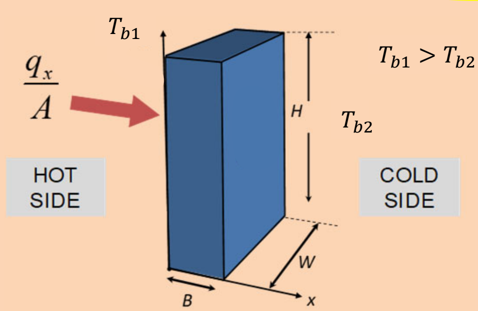
To get started, let's contrast the **steady** and **unsteady** cases in a familiar problem:

HEAT TRANSFER

Steady vs. **Unsteady**

1D, heat conduction, in the x-direction, in a slab

Newton's law of Cooling boundary conditions



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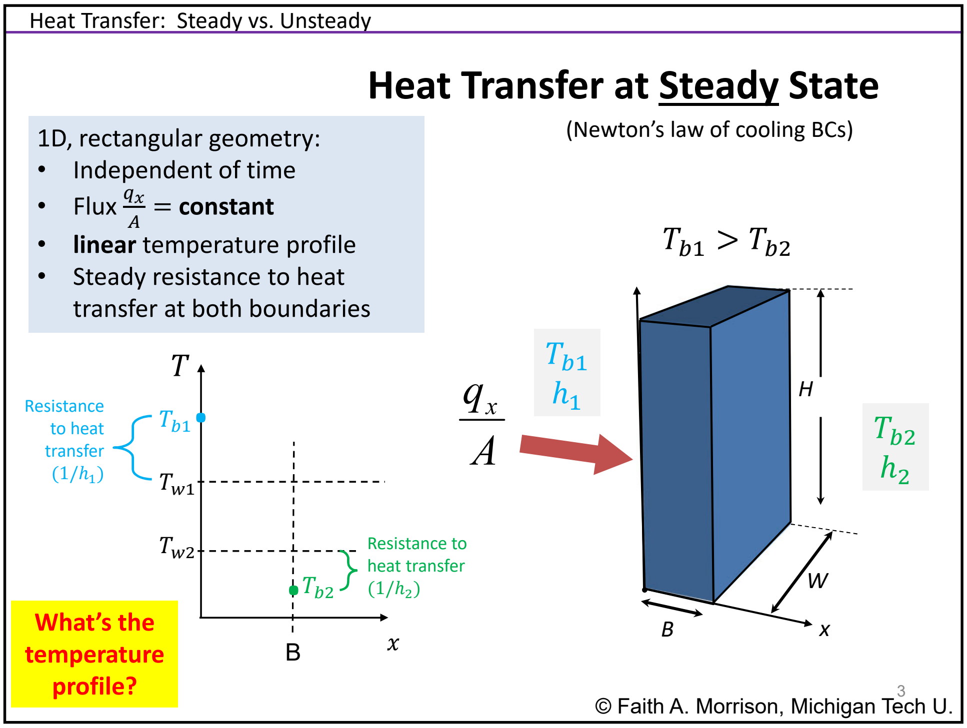
Heat Transfer: Steady vs. Unsteady
Heat Transfer at Steady State
(Newton's law of cooling BCs)
1D, rectangular geometry:
• Independent of time
• Flux $\frac{q_x}{A}$ = constant
• linear temperature profile
• Steady resistance to heat transfer at both boundaries
$T_{b1} > T_{b2}$
T
Resistance to heat transfer $(1/h_1)$
T_{b1}
T_{w1}
T_{w2}
T_{b2}
Resistance to heat transfer $(1/h_2)$
B
x
What's the temperature profile?
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
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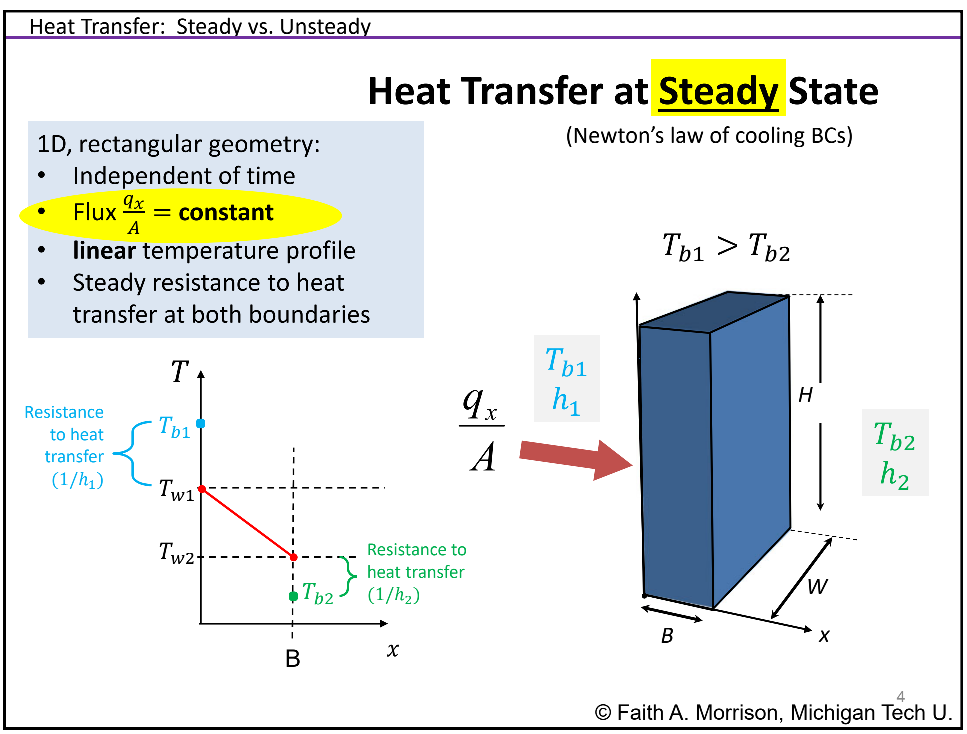
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T_{b1} h_1
T_{b2} h_2
H
W
B
x
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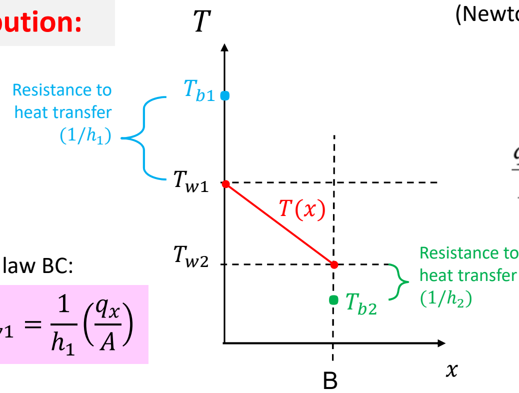
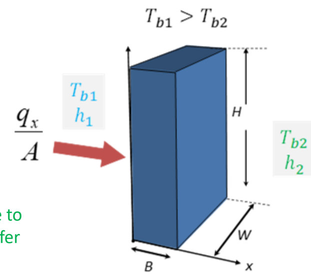
Heat Transfer: Steady vs. Unsteady

Heat Transfer at Steady State

(Newton's law of cooling BCs)

Temperature distribution:





Newton's law BC:

$$T_{b1} - T_{w1} = \frac{1}{h_1}\left(\frac{q_x}{A}\right)$$

$$\frac{q_x}{A} = h_1(T_{b1} - T_{w1}) = -k\frac{dT}{dx} = h_2\,(T_{w2} - T_{b2})$$

Flux $\frac{q_x}{A}$ = constant

Independent of time

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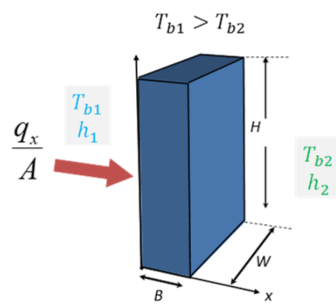
Heat Transfer: Steady vs. Unsteady

Unsteady Heat Transfer



There are many circumstances that cause unsteady heat transfer.

To imagine a case where heat transfer is unsteady:

- We must specify the state of the system at some point in time (***initial conditions***)
- We must specify what then happens to cause heat to start to transfer (**the scenario**).

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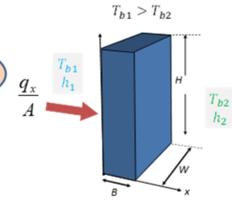
Heat Transfer: Steady vs. Unsteady

Unsteady Heat Transfer

There are many circumstances that cause unsteady heat transfer.



To imagine a case where heat transfer is unsteady:

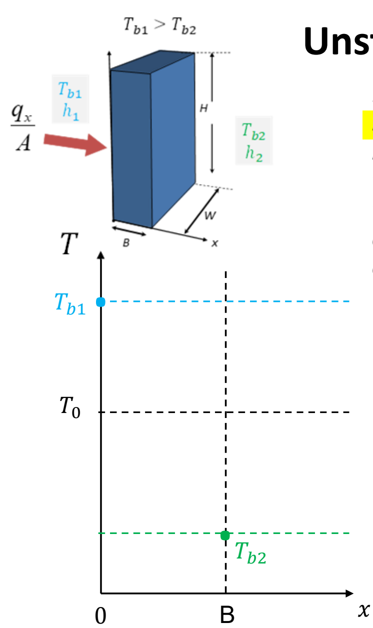
- We must specify the state of the system at some point in time (***initial conditions***)
- We must specify what then happens to cause heat to start to transfer (**the scenario**).

Can you think of any real engineering situations (unsteady heat xfer)?
Can you write them in terms of:
- **initial conditions and**
- **a modeling scenario?**

You try.

Heat Transfer: Steady vs. Unsteady

Unsteady Heat Transfer

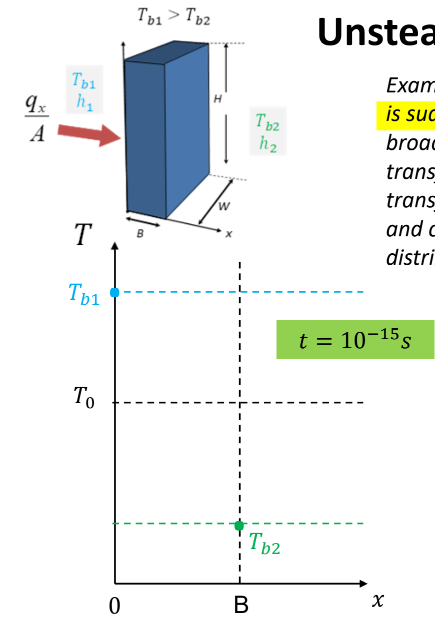


Example: A wide, tall slab initially uniformly at T_0 is suddenly subjected to flowing fluid on its two broad faces. The left fluid is at T_{b1} and its heat transfer to the wall is characterized by heat transfer coefficient h_1, while the right side is at T_{b2} and characterized by h_2. What is the temperature distribution across the slab as a function of time?

What do we think will happen?
- Will there be heat transfer resistance at the boundaries?
- Will there be a linear temperature profile in the slab?
- Femtoseconds after the change, what does the profile look like?
- What will the solution trend towards as time goes on ($\rightarrow \infty$)?

Heat Transfer: Steady vs. Unsteady

Unsteady Heat Transfer



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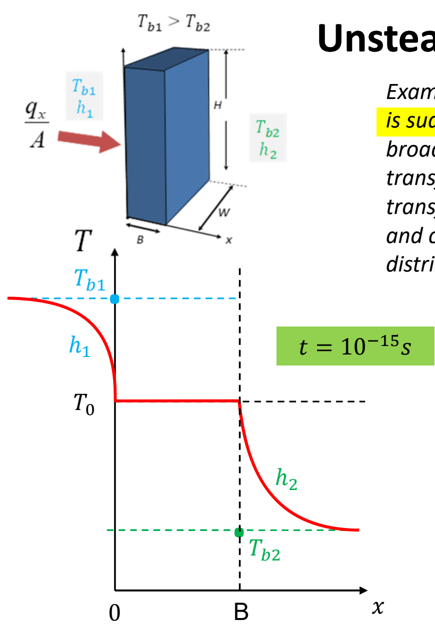
What do we think will happen?

You try.

$femtosecond = 10^{-15} s$

Heat Transfer: Steady vs. Unsteady

Unsteady Heat Transfer



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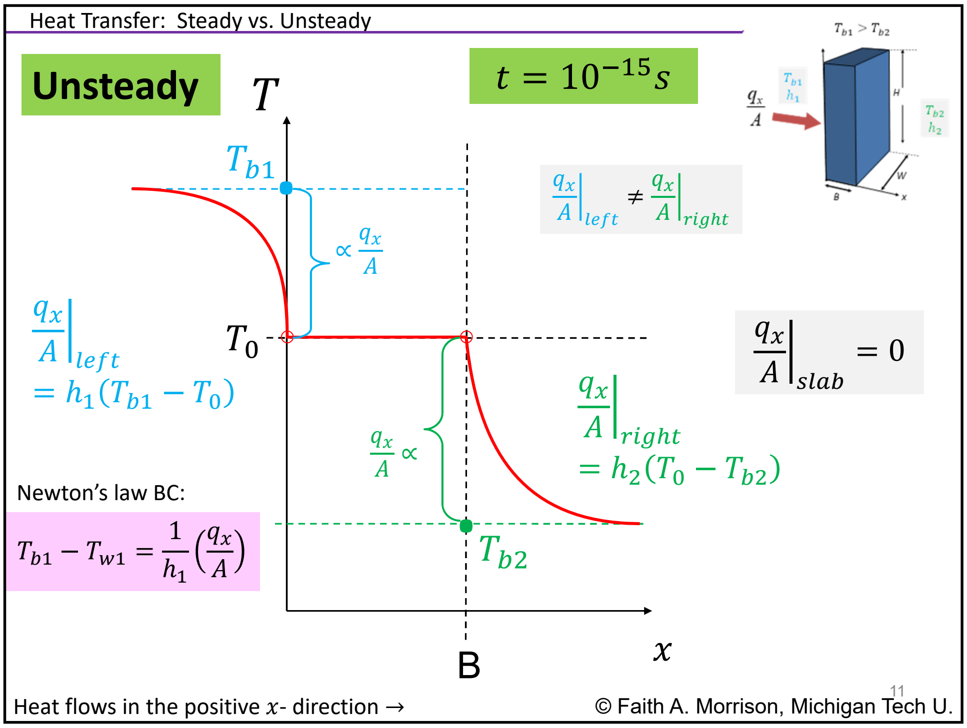
Heat Transfer: Steady vs. Unsteady
Unsteady
$t = 10^{-15} s$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} \neq \left.\frac{q_x}{A}\right|_{right}$
$\left.\frac{q_x}{A}\right|_{slab} = 0$
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_0)$
T_0
$\frac{q_x}{A} \propto$
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_0 - T_{b2})$
Newton's law BC:
$T_{b1} - T_{w1} = \frac{1}{h_1}\left(\frac{q_x}{A}\right)$
T_{b2}
B
x
Heat flows in the positive x- direction →
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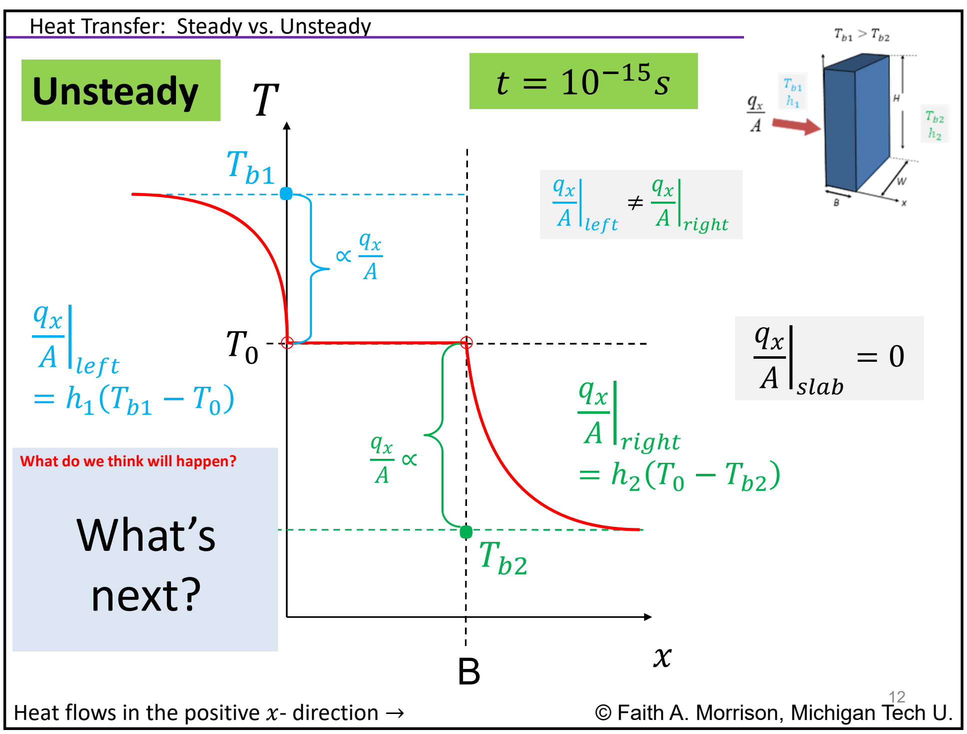
Heat Transfer: Steady vs. Unsteady
Unsteady
$t = 10^{-15} s$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} \neq \left.\frac{q_x}{A}\right|_{right}$
$\left.\frac{q_x}{A}\right|_{slab} = 0$
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_0)$
T_0
What do we think will happen?
What's next?
$\frac{q_x}{A} \propto$
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_0 - T_{b2})$
T_{b2}
B
x
Heat flows in the positive x- direction →
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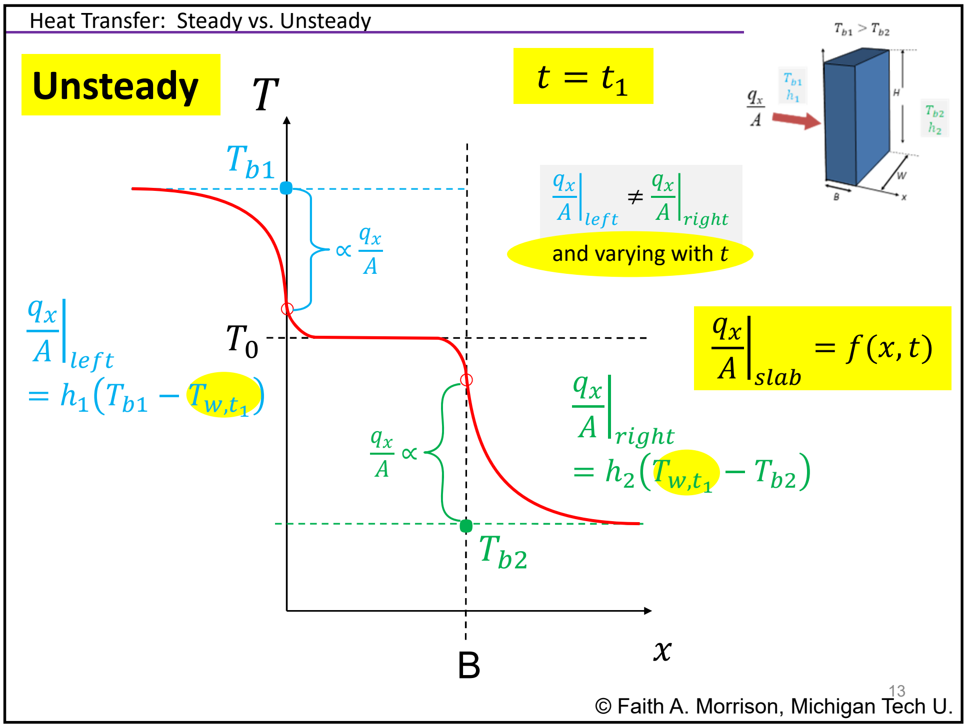
Heat Transfer: Steady vs. Unsteady
Unsteady
$t = t_1$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} \neq \left.\frac{q_x}{A}\right|_{right}$
and varying with t
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_{w,t_1})$
T_0
$\left.\frac{q_x}{A}\right|_{slab} = f(x,t)$
$\frac{q_x}{A} \propto$
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_{w,t_1} - T_{b2})$
T_{b2}
B
x
13
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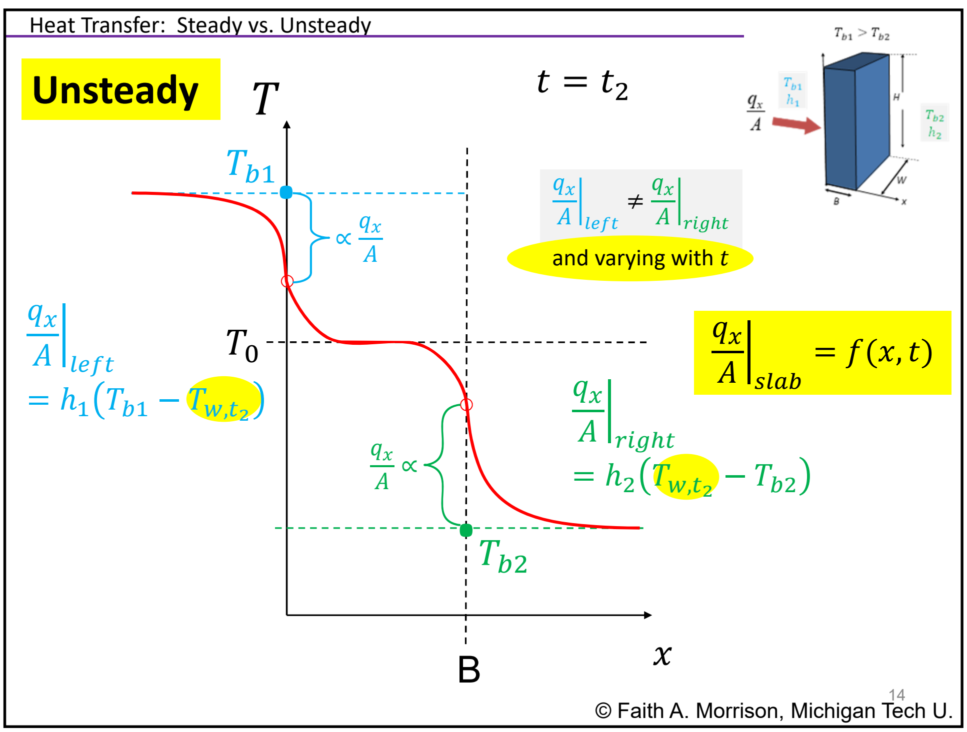
Heat Transfer: Steady vs. Unsteady
Unsteady
$t = t_2$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} \neq \left.\frac{q_x}{A}\right|_{right}$
and varying with t
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_{w,t_2})$
T_0
$\left.\frac{q_x}{A}\right|_{slab} = f(x,t)$
$\frac{q_x}{A} \propto$
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_{w,t_2} - T_{b2})$
T_{b2}
B
x
14
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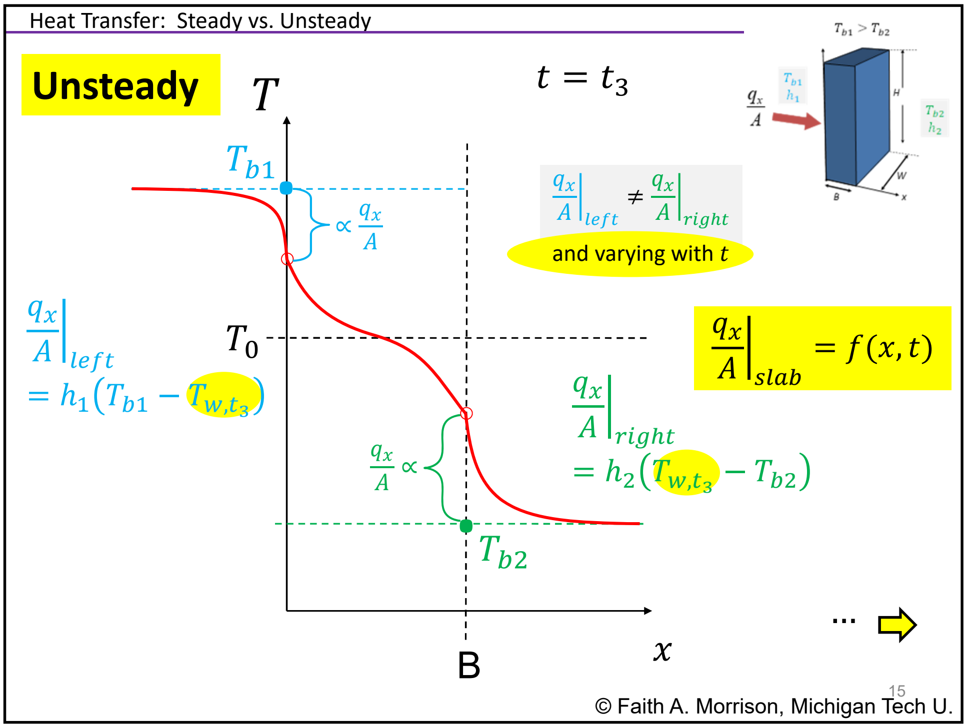
Heat Transfer: Steady vs. Unsteady
Unsteady
$t = t_3$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} \neq \left.\frac{q_x}{A}\right|_{right}$
and varying with t
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_{w,t_3})$
T_0
$\left.\frac{q_x}{A}\right|_{slab} = f(x,t)$
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_{w,t_3} - T_{b2})$
$\frac{q_x}{A} \propto$
T_{b2}
B
x
…
15
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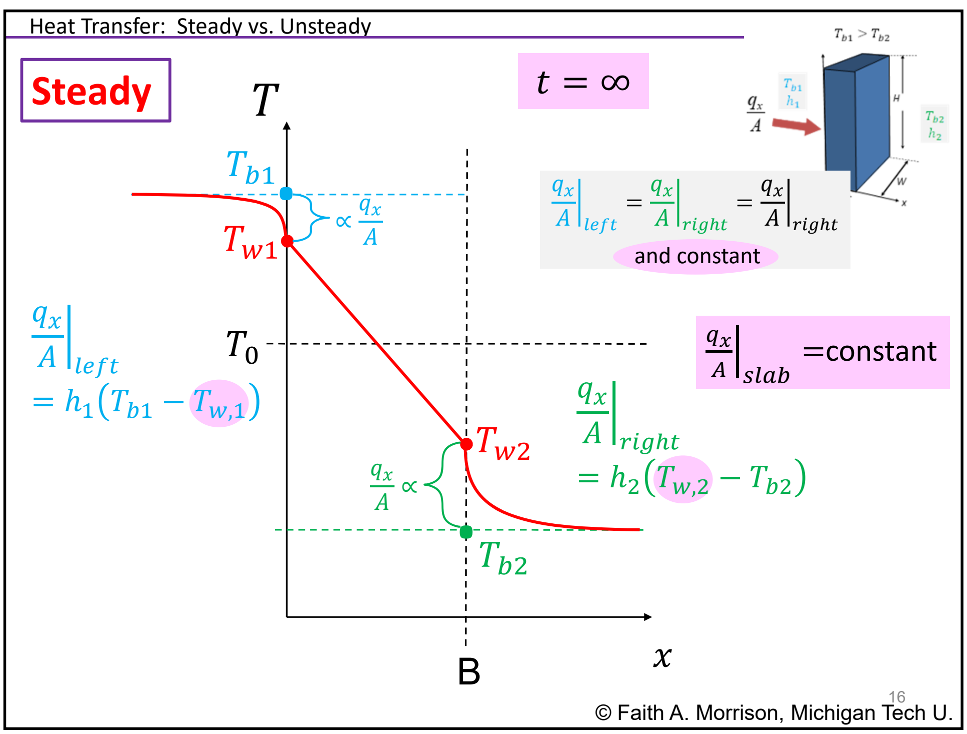
Heat Transfer: Steady vs. Unsteady
Steady
$t = \infty$
$T_{b1} > T_{b2}$
$\frac{q_x}{A}$
T_{b1} h_1
T_{b2} h_2
H
W
B
x
T
T_{b1}
T_{w1}
$\propto \frac{q_x}{A}$
$\left.\frac{q_x}{A}\right|_{left} = \left.\frac{q_x}{A}\right|_{right} = \left.\frac{q_x}{A}\right|_{right}$
and constant
$\left.\frac{q_x}{A}\right|_{left} = h_1(T_{b1} - T_{w,1})$
T_0
$\left.\frac{q_x}{A}\right|_{slab}$ =constant
T_{w2}
$\left.\frac{q_x}{A}\right|_{right} = h_2(T_{w,2} - T_{b2})$
$\frac{q_x}{A} \propto$
T_{b2}
B
x
16
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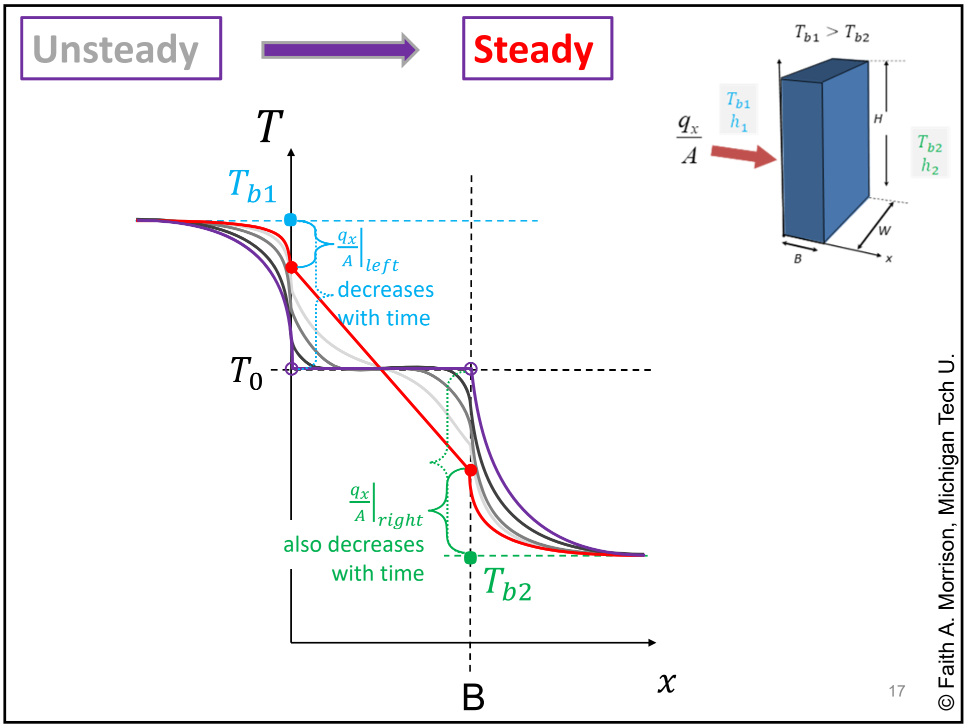
Unsteady
Steady
$T_{b1} > T_{b2}$
T_{b1} h_1
T_{b2} h_2
$\frac{q_x}{A}$
H
W
B
x
T
T_{b1}
$\frac{q_x}{A}\Big|_{left}$ decreases with time
T_0
$\frac{q_x}{A}\Big|_{right}$ also decreases with time
T_{b2}
B
x
17
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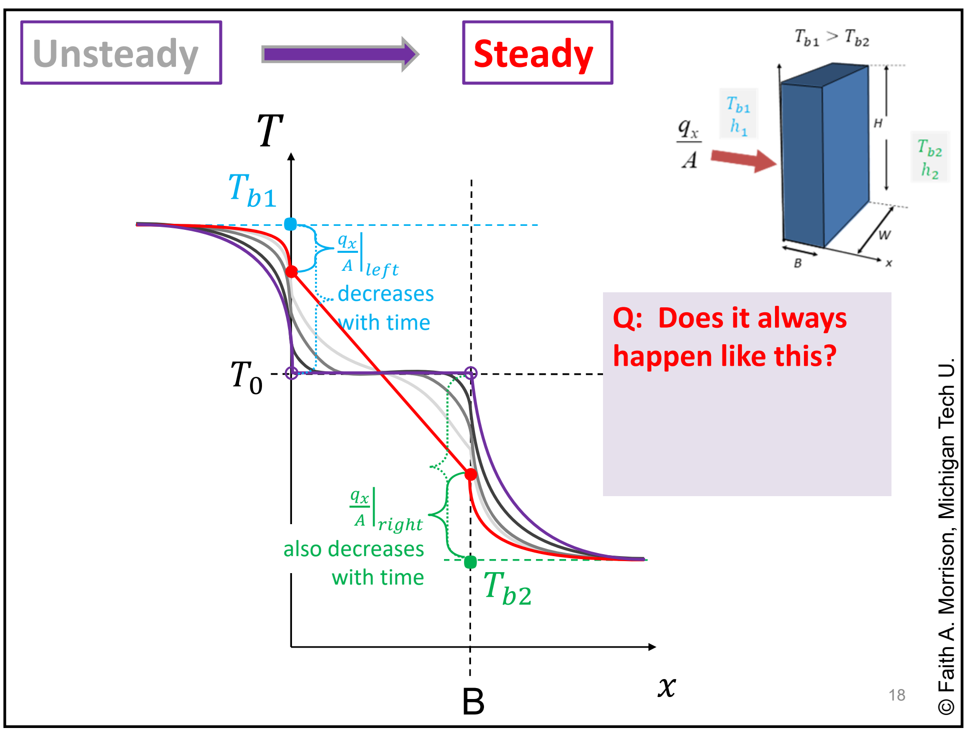
Unsteady
Steady
$T_{b1} > T_{b2}$
T_{b1} h_1
T_{b2} h_2
$\frac{q_x}{A}$
H
W
B
x
T
T_{b1}
$\frac{q_x}{A}\Big|_{left}$ decreases with time
T_0
Q: Does it always happen like this?
$\frac{q_x}{A}\Big|_{right}$ also decreases with time
T_{b2}
B
x
18
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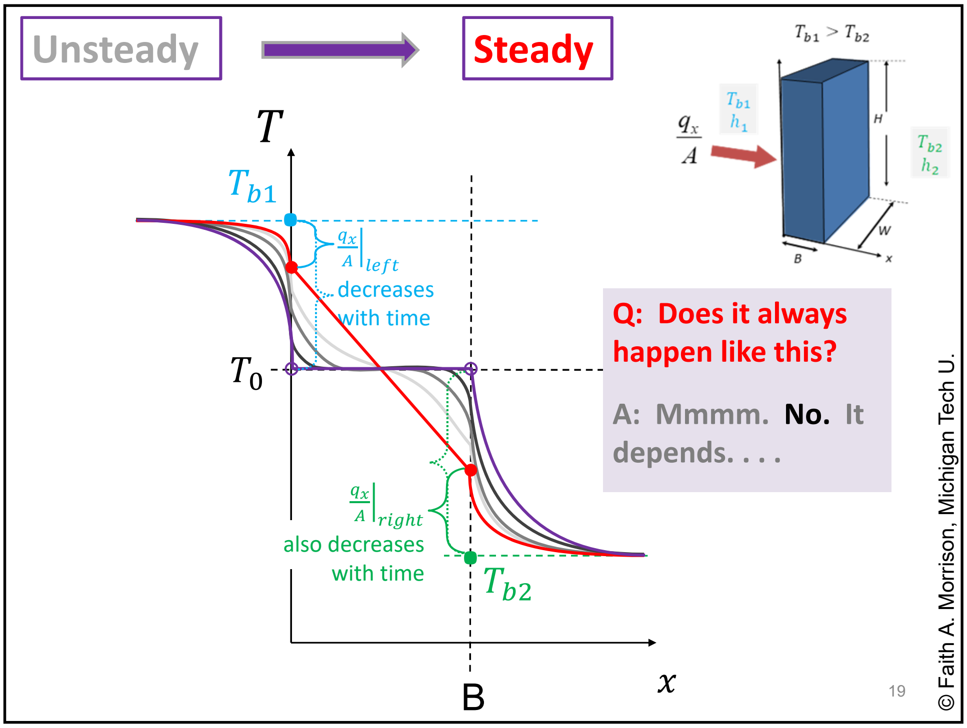
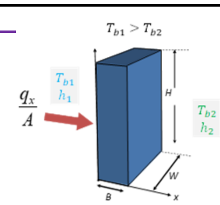


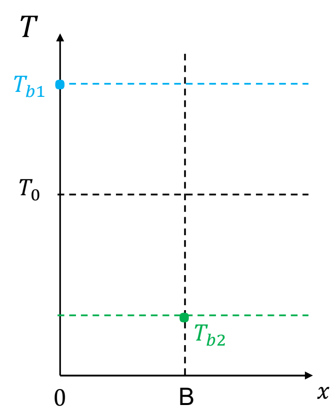
Heat Transfer: Steady vs. Unsteady

What are the various cases that are seen?

- h_i are large



Let's think.



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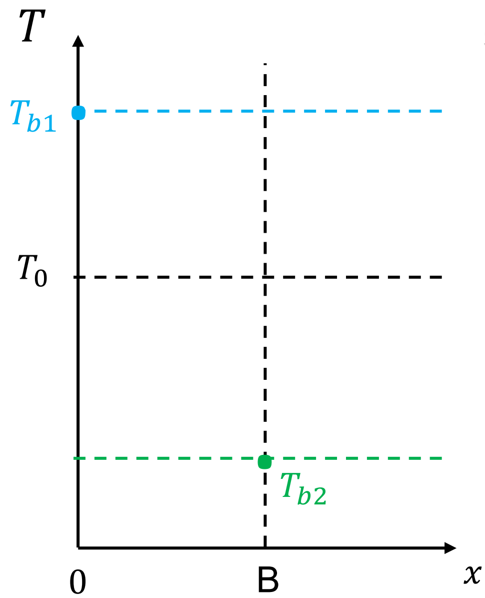
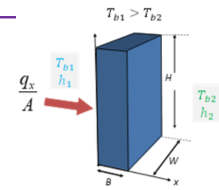
Heat Transfer: Steady vs. Unsteady

- h_i are large





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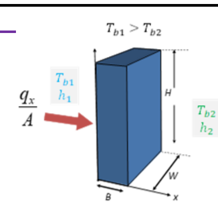
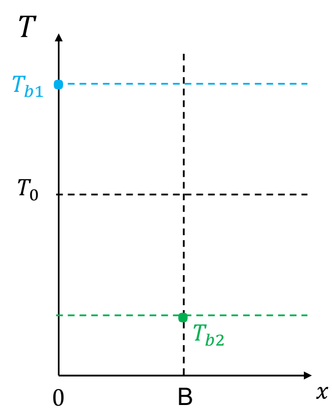
Heat Transfer: Steady vs. Unsteady

What are the various cases that are seen?

- k is large

Let's think.





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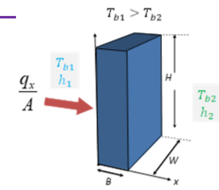
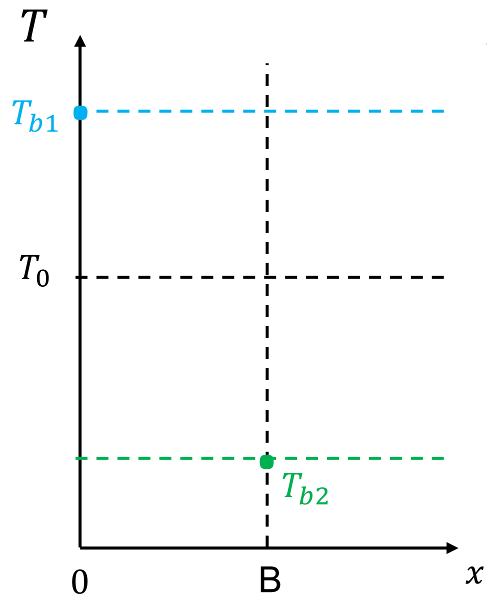
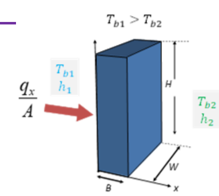
Heat Transfer: Steady vs. Unsteady



- k is large



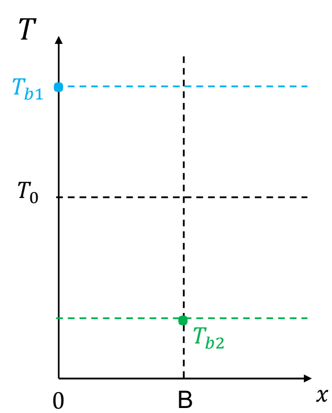
Heat Transfer: Steady vs. Unsteady



What are the various cases that are seen?

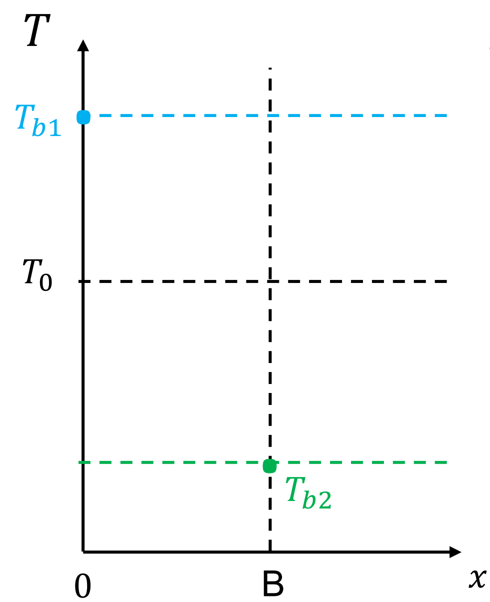
- Neither slab conduction nor fluid convection dominates

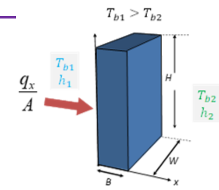
Let's think.



Heat Transfer: Steady vs. Unsteady

- Neither slab conduction nor fluid convection dominates





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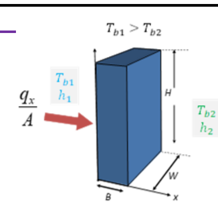
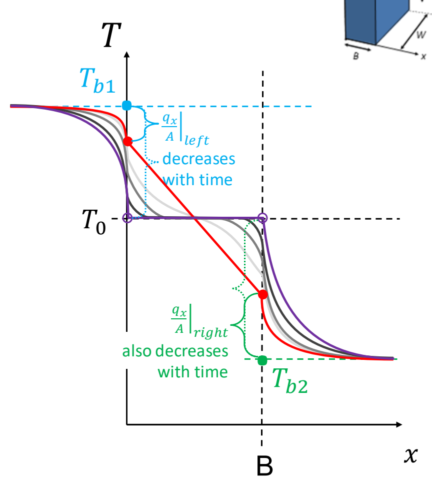
Heat Transfer: Steady vs. Unsteady

What are the various cases that are seen?

- If h_i is large, the wall temp is just the bulk temperature (fast convection)
- If k is large, the temp profile is always straight (quasi-steady state in the slab) and the convection works to keep up (heat transfer is limited by h_i; fast conduction in slab)
- If neither mechanism dominates, it's complicated!
- If the boundary conditions vary with $t, \underline{x}$, it's complicated!





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Heat Transfer: Steady vs. Unsteady

What is our usual strategy for complex phenomena?

Answer: Dimensional Analysis

CM3110: Momentum and Heat Xfer

Complex Heat Transfer – Dimensional Analysis

Experience with Dimensional Analysis (momentum):

- Flow in pipes at all flow rates (laminar and turbulent)
  Solution: Navier-Stokes, Re, Fr, L/D, dimensionless wall force $= f$; $f = f(\mathrm{Re}, L/D)$
- Rough pipes — ***Solution:*** add additional length scale; then nondimensionalize
- Non-circular conduits — ***Solution:*** Use hydraulic diameter as the length scale of the flow to nondimensionalize
- Flow around obstacles (spheres, other complex shapes
  Solution: Navier-Stokes, Re, dimensionless drag $= C_D$; $C_D = C_D(\mathrm{Re})$
- Boundary layers — ***Solution:*** Two components of velocity need independent lengthscales

Let's review

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