

Ch9; Thermal Conductivity and Mechanisms of Energy Transport.

Mechanisms of Energy Transport

1. molecular energy transport - due to molecular motion
2. convective " " - due to bulk fluid motion
3. diffusive " " - due to interdiffusing mixtures (ch 19.3, 24.2).
4. radiation " " - ch 16.

Molecular Energy Transport. - Conduction

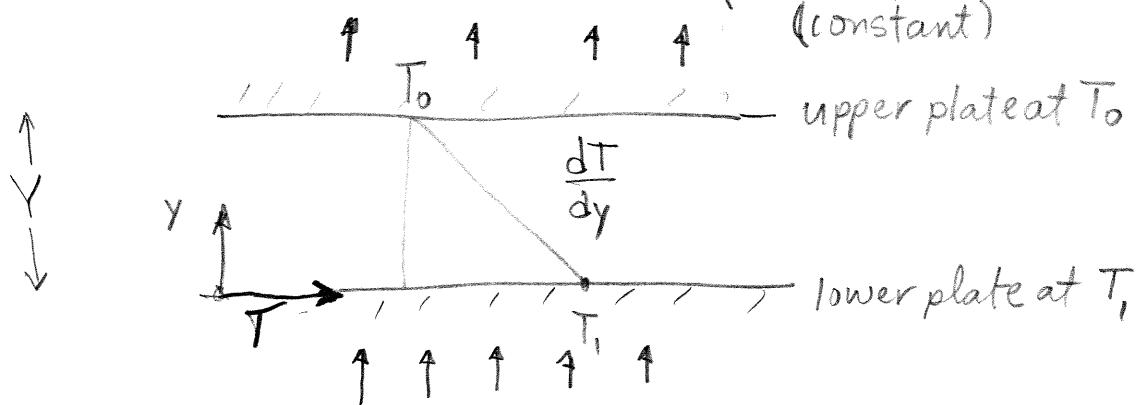
→ conduction of heat is a familiar concept to everyone

examples: a) holding a cold metal object vs
a " wood "

b) "wet" cloths feel colder than dry cloths

c) cooking items like pots + pans are often fabricated with a layer of Cu or Al to distribute heat.

Fourier's Law of Conduction: $Q = \text{rate of heat flow}$
(constant)



observed. $\frac{Q}{A} = k \frac{\Delta T}{Y}$ "Fourier's Law"

more accurately; $q_y = -k \frac{dT}{dy}$ "

where q_y = flux of heat in positive y direction.

$\frac{dT}{dy}$ = temperature gradient in the y direction

If k = thermal conductivity [$W/(m \cdot K)$] or [$\text{cal}/(\text{cm} \cdot \text{s} \cdot ^\circ\text{C})$]

temperature gradients exist in 3 coordinate directions

$$q_x = -k \frac{dT}{dx}, \quad q_y = -k \frac{dT}{dy}, \quad q_z = -k \frac{dT}{dz}$$

When the unit vector, δ_i , is (x) and 3 components \vec{q}

$$\boxed{q = -k \nabla T}$$

q is a heat flux vector.
 ∇T is a gradient vector.

and k is the same in all 3 coordinate directions,

isotropic

For anisotropic materials (noncubic crystals, fibrous materials, laminates)

$$q = -[K \cdot \nabla T]$$

where K (κ) is the thermal conductivity tensor.

Thus, the heat flux vector does not point in the same direction as the temperature gradient.

Another important energy (heat) transport property is.

$$\alpha = \frac{k}{\rho \hat{C}_p} \quad [m^2/s] \text{ or } [cm^2/sec]. \quad \text{"thermal diffusivity"}$$

Where ρ = material density [g/cm^3]

\hat{C}_p = heat capacity at constant pressure [$cal/(^{\circ}C \cdot g)$]

A dimensionless number often appearing in equation of change for energy transport is.

$$Pr \equiv \frac{\nu}{\alpha} = \frac{\hat{C}_p \mu}{k} \quad \text{"Prandtl number"}$$

$$Pe \equiv Re Pr \quad \text{"Peclet number"}$$

Summary of k , Pr values. Tables 9.1-2 - 9.1-5

gases: $0.01 \leq k \leq 0.10 \quad [W/m \cdot K]$

liquids: $0.10 \leq k \leq 1.0 \quad "$

liquid metals: $10 \leq k \leq 100 \quad "$

solids: $0.01 \leq k \leq 1,000 \quad "$

Temperature Dependence of k

gases: $k \uparrow$ with $\uparrow T$

liquids: $k \downarrow$ with $\uparrow T$

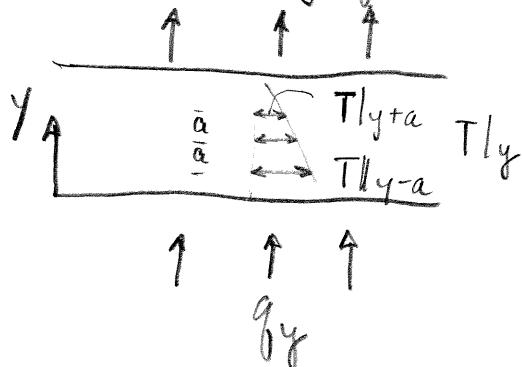
solids: $k \uparrow$ with $\uparrow T$

Pressure Dependence of k ,

gases: $k \uparrow$ when $P \uparrow$

liquids: $k \uparrow$ as $P \uparrow$

Kinetic Theory of Gas: Prediction of k .



Energy Balance at y :

"heat flux across any plane at y " =

"rate of kinetic energy arriving
from a plane at $y-a$ " -

"rate of kinetic energy arriving
from a plane at $y+a$ "

properties of a monatomic gas,

$$\bar{u} = \sqrt{\frac{8kT}{\pi m}}$$

$$Z = \frac{1}{4} n \bar{u} \quad \text{collision frequency}$$

$$\lambda = \frac{1}{\sqrt{2\pi d^2 n}} \quad \text{mean free path}$$

$$\frac{1}{2} m \bar{u}^2 = \frac{3}{2} kT \quad \text{mean kinetic energy/molec.}$$

$$a = \frac{2}{3} \lambda \quad \begin{array}{l} \text{avg. distance} \\ \text{between planes} \\ \text{where last col-} \\ \text{lision occurred} \end{array}$$

$$q_y = Z \frac{1}{2} m \bar{u}^2 |_{y-a} - Z \frac{1}{2} m \bar{u}^2 |_{y+a}$$

$$\zeta = Z \left(\frac{3}{2} k T |_{y-a} - \frac{3}{2} k T |_{y+a} \right) = \frac{3}{2} k Z (T|_{y-a} - T|_{y+a})$$

$$T|_{y-a} = T|_y - a \frac{dT}{dy} = T|_y - \frac{2}{3} \lambda \frac{dT}{dy}$$

$$T|_{y+a} = T|_y + a \frac{dT}{dy} = T|_y + \frac{2}{3} \lambda \frac{dT}{dy}$$

$$q_y = \frac{3}{2} K Z \left(T|_y - \frac{2}{3} \lambda \frac{dT}{dy} - T|_y + \frac{2}{3} \lambda \frac{dT}{dy} \right).$$

$$= -2 K Z \lambda \frac{dT}{dy}$$

$$= -2 K^2 \left(\frac{1}{4} \pi \bar{u} \right) \left(\frac{1}{\sqrt{2} \pi d^2} \right) \frac{dT}{dy}$$

$$= -2 K \left(\frac{1}{4} \sqrt{\frac{8 K T}{\pi m}} \right) \left(\frac{1}{\sqrt{2} \pi d^2} \right) \frac{dT}{dy}$$

$$= - \frac{2}{4} \frac{\sqrt{8}}{\sqrt{2}} \left(\frac{\sqrt{K T / (\pi m)}}{\pi d^2} \right) \lambda \frac{dT}{dy}$$

$$= - \left(\frac{\sqrt{K m T / \pi}}{\pi d^2} \right) \frac{K}{m} \frac{dT}{dy}$$

$$= - \frac{2}{3\pi} \frac{\sqrt{\pi m K T}}{\pi d^2} \hat{C}_v \frac{dT}{dy}.$$

$$\text{where } \hat{C}_v = \frac{3}{2} \frac{K}{m}$$

heat capacity at
constant volume per
mole gas.

From Fourier's Law,

$$q_y = -k \frac{dT}{dy}$$

$$\therefore \boxed{k = \frac{2}{3\pi} \frac{\sqrt{\pi m K T}}{\pi d^2} \hat{C}_v}$$

Chapman-Enskog Formula:

$$k = \frac{25}{35} \frac{\sqrt{\pi m k T}}{\pi \sigma^2 \Omega_k} \hat{C}_v \text{ or } k = 1.9891 \times 10^{-4} \frac{\sqrt{T/M}}{\sigma^2 \Omega_k}$$

\uparrow
 $[\text{cal}/(\text{cm.s.K})]$

$T [{}^\circ\text{K}]$

$\sigma [\text{\AA}]$

$\Omega_k = \Omega_u \text{ in Eq. 2.}$

$$k = \frac{15}{4} \frac{R}{M} \mu = \frac{5}{2} \hat{C}_v \mu \quad \text{from Eqn. 9.3-13}$$

and " 1.4-14.

Other Useful Formula, for Polyatomic gases.

$$k = (\hat{C}_p + \frac{5}{4} \frac{R}{M}) \mu \quad \hat{C}_p = \frac{5}{2} \frac{R}{M} \text{ for monatomic gases.}$$

$$P_r \equiv \frac{\hat{C}_p \mu}{k} = \frac{\hat{C}_p}{(\hat{C}_p + \frac{5}{4} R)}$$

Wed 2/22/06

Bridgman's Theory; monatomic liquids,

Assumptions:

- atoms/molecules oscillate inside a "cage" having a volume roughly $= \tilde{V}/\tilde{N}$ volume/mole
avogadro's no.
- heat transferred by collisions with nearest neighbor molecules at the sonic velocity of the liquid, $v_s = \sqrt{\frac{C_p}{C_v}} \left(\frac{\partial P}{\partial \rho} \right)_T$ isothermal compressibility.
 ~ 1 for liquids

$$k = \frac{1}{3} \rho \hat{C}_v \bar{u} \lambda = \rho \hat{C}_v |u| \lambda$$

molecular mass $\frac{m \tilde{N}}{\tilde{V}}$ $3 \frac{K}{m}$ v_s spacing between lattice planes in the liquid. $(\tilde{V}/\tilde{N})^{1/3}$.
 Boltzmann's Constant

$$k = 3 (\tilde{N}/\tilde{V})^{2/3} K v_s \rightarrow \boxed{2.8 (\tilde{N}/\tilde{V})^{2/3} K v_s}$$