

# Generalizations of Newton's Law of Viscosity, 1.2

in simple, steady-state shearing flow

$$\tau_{ij} = -\mu \frac{\partial v_j}{\partial x_i} \quad \text{where } j = \text{one coord-direction} \\ i = \text{another " " "}$$

as shown in Section 1.1!

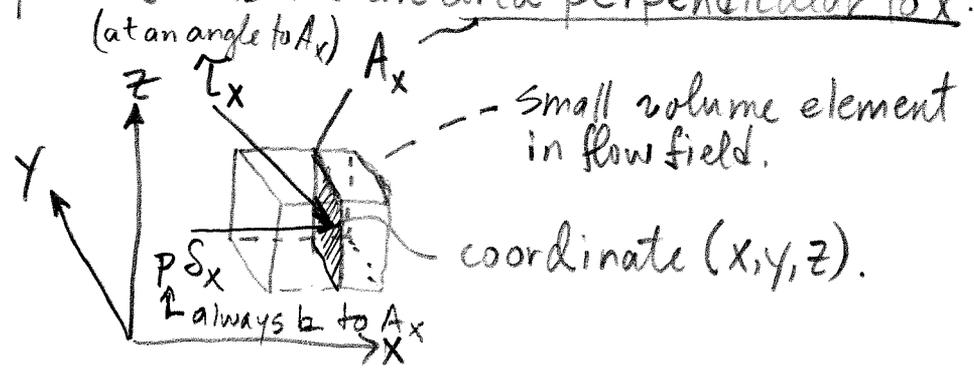
Most real flows are much more complicated where each component of velocity varies with time + space.

$$v_x(x, y, z, t) \quad v_y(x, y, z, t) \quad v_z(x, y, z, t)$$

Nine stress components will result from this general flow configuration.

For example - forces on an area perpendicular to x.

"remove  $\frac{1}{2}$  of fluid in the cube!  $\tau_x$  and  $p \delta_x$  are the forces / area ( $A_x$ ) to replace this fluid."



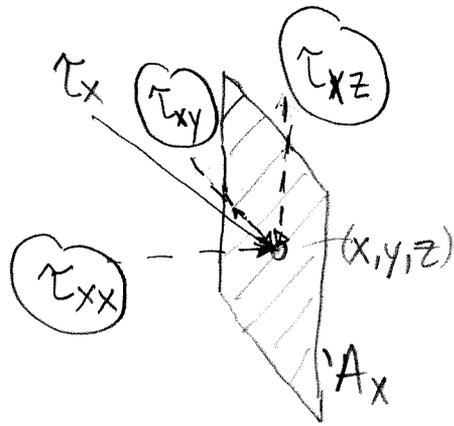
$p \delta_x$  is pressure stress acting normal to  $A_x$

$\delta_x$  is a unit vector normal to  $A_x$ .

$p$  is thermodynamic pressure of the fluid at  $(x, y, z)$ .

$\tau_x$  is viscous force/unit area (stress) due to velocity gradients acting on  $A_x$ .

$\tau_x$  is a vector with components,



all which exert a force per unit area on  $A_x$  in the fluid due to velocity gradients in the fluid.

Thus, there are 9 viscous stress components, 3 each exerting a force on each area,  $A_x$ ,  $A_y$ , and  $A_z$ .

Molecular Stress is the sum of pressure + viscous stress.

$$\hat{\Pi}_{ij} = p \delta_{ij} + \tilde{\tau}_{ij}$$

where  $i$  and  $j$  may be  $x, y, \text{ or } z$ .

where

$$\begin{aligned} \delta_{ij} &\equiv \text{Kronecker delta} = 0 \text{ for } i \neq j \\ &= 1 \text{ for } i = j \end{aligned}$$

normal stresses,  $\hat{\Pi}_{ii} = p + \tilde{\tau}_{ii}$

shear stresses,  $\hat{\Pi}_{ij} = \tilde{\tau}_{ij} \quad i \neq j$

Table 1.2-1 for a summary of Molecular Stress Tensor

How are  $\tau_{ij}$  related to velocity gradients?

$$\tau_{ij} = -\mu \left( \frac{\partial v_j}{\partial x_i} + \frac{\partial v_i}{\partial x_j} \right) + \left( \frac{2}{3}\mu - k \right) \left( \frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} \right) \delta_{ij}$$

where

$k$  = dilatational viscosity  
 = 0 for ideal monoatomic gases.  
 assumed 0 for real gases.

see  
 Appendix  
 B

note 2 properties,  $\mu$  and  $k$

In Tensor Notation.

$$\tau = -\mu (\nabla \mathbf{v} + (\nabla \mathbf{v})^t) + \left( \frac{2}{3}\mu - k \right) (\nabla \cdot \mathbf{v}) \delta$$

Appendix A  $\left\{ \begin{array}{l} \delta = \text{unit tensor} \\ \nabla \mathbf{v} = \text{velocity gradient tensor} \\ (\nabla \mathbf{v})^t = \text{transpose of } \nabla \mathbf{v} \\ \nabla \cdot \mathbf{v} = \text{"divergence" of velocity vector.} \end{array} \right.$

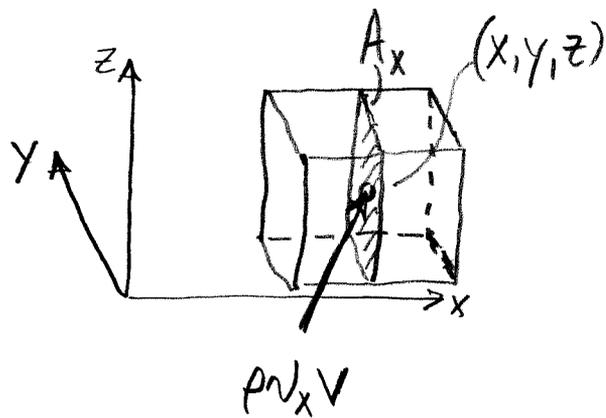
note: Ch 3 we show that incompressible fluids,

$$(\nabla \cdot \mathbf{v}) = 0 \quad \therefore \text{so } k \text{ term} \equiv 0!$$

$k$  is useful / important for

- sound absorption in polyatomic gases
- fluid flow containing gas bubbles.

## Convective Momentum Transport, 1.7



$v_x =$   $x$  component of velocity vector  
(volumetric flow / unit area,  $A_x$ ).

$v =$  velocity vector

$\rho v =$  momentum / unit volume - a vector quantity.

$\rho =$  fluid density.

$\rho v_x v =$  flux of momentum from regions of lesser  $x$   
to regions of greater  $x$  by bulk flow  
(convection) through  $A_x$ .

3 components;  $\rho v_x v_x$ ,  $\rho v_x v_y$ ,  $\rho v_x v_z$

For each of the other unit areas,  $A_y$  &  $A_z$ , there are  
3 momentum flux components

Table 1.7-1 is a summary of the Convective Momentum  
Flux Components.

## Combined Momentum Flux Tensor, $\Phi$

$$\Phi = \overset{\uparrow}{\Pi} + \rho \underset{\swarrow}{V} V = p \delta + \tilde{\tau} + \rho V V$$

molecular momentum flux tensor	Convective Momentum Flux Tensor
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$$\Phi_{xx} = \Pi_{xx} + \rho v_x v_x = p + \tilde{\tau}_{xx} + \rho v_x v_x$$

$$\Phi_{xy} = \Pi_{xy} + \rho v_x v_y = \tilde{\tau}_{xy} + \rho v_x v_y$$

"combined flux of y-momentum through a surface perpendicular to x-direction,  $A_x$ ."