

3.6 Uses of Equations of Change.

steady Flow in a Long Circular Tube.
 ρ, μ constant

$$V = \delta_z v_z(r, z)$$

$$v_r = v_\theta = 0$$

Eqn. of Continuity: Table B.4

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (\rho r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho r v_\theta) + \frac{\partial}{\partial z} (\rho v_z) = 0$$

$$\rho \frac{\partial v_z}{\partial z} + v_z \frac{\partial \rho}{\partial z} = 0 \Rightarrow \boxed{\frac{\partial v_z}{\partial z} = 0} \quad \text{"} V = \delta_z v_z(r) \text{"}$$

only "

Eqn. of Motion: Table B.6

$$\begin{aligned} \Phi = P(z) \text{ alone} \left\{ \begin{array}{l} r\text{-component} \Rightarrow 0 = -\frac{\partial P}{\partial r} + \rho g_r \text{ or } \boxed{0 = -\frac{\partial \Phi}{\partial r}} \\ \theta\text{-component} \Rightarrow 0 = -\frac{1}{r} \frac{\partial P}{\partial \theta} + \rho g_\theta \text{ or } 0 = -\frac{\partial P}{\partial \theta} + \rho g_\theta \\ \boxed{0 = -\frac{\partial \Phi}{\partial \theta}} \end{array} \right. \end{aligned}$$

$$z\text{-component} \Rightarrow 0 = -\frac{\partial P}{\partial z} + \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right)$$

$$0 = -\frac{\partial P}{\partial z} + \mu \frac{1}{r} \frac{d}{dr} \left(r \frac{dv_z}{dr} \right) \Rightarrow v_z = v_z(r)$$

$$\mu \frac{1}{r} \frac{d}{dr} \left(r \frac{dv_z}{dr} \right) = C_0 = \frac{dP}{dz}$$

$C_0 = \text{constant.}$

$$\therefore P = C_0 z + C_1$$

$$v_z = \frac{C_0}{4\mu} r^2 + C_2 \ln r + C_3$$

$$\begin{array}{llll}
 \text{BC1} & z=0 & P=P_0 & \rightarrow C_1=P_0 \\
 \text{BC2} & z=L & P=P_L & \rightarrow C_0=(P_L-P_0)/L \\
 \text{BC3} & r=R & v_z=0 & \rightarrow C_3=\frac{P_0-P_L R^2}{4\mu L} \\
 \text{BC4} & r=0 & v_z=\text{finite} & \rightarrow C_2=0
 \end{array}$$

$$P = P_0 - (P_0 - P_L) (z/L)$$

$$v_z = \frac{P_L - P_0}{4\mu L} r^2 + \frac{P_0 - P_L}{4\mu L} R^2$$

$$= \frac{(P_0 - P_L) R^2}{4\mu L} \left(1 - \left(\frac{r}{R}\right)^2\right)$$

$$\begin{aligned}
 \tau_{rz} &= -\mu \frac{\partial v_z}{\partial r} \\
 &= \frac{\mu(P_0 - P_L)}{2\mu L} r
 \end{aligned}$$

$$\tau_{rz, \max} = \frac{(P_0 - P_L) R}{2L}$$

$$\begin{aligned}
 F_z &= \text{Shear force of fluid on wall} \\
 &= (2\pi RL) \tau_{rz, \max}
 \end{aligned}$$

Falling Film Problem.

$$v_z = v_z(x) \quad \rho = \text{constant}$$

$$v_x = v_y = 0 \rightarrow \text{Table B.1} \quad \tau_{zx} = \tau_{xz} = -\mu \frac{\partial v_z}{\partial x}$$

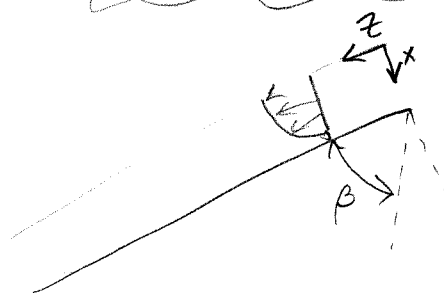
Eqn. of Continuity: $\Rightarrow$ all terms are zero

Egns. of Motion: in terms of τ Table B.5

$$x\text{-component: } 0 = -\frac{\partial P}{\partial x} + \rho g \sin \beta$$

$$y\text{-component: } 0 = -\frac{\partial P}{\partial y} \quad P \neq P(y)$$

$$z\text{-component: } 0 = -\frac{\partial P}{\partial z} - \frac{\partial}{\partial x} \tau_{xz} + \rho g \cos \beta$$



integrating x-component eqn,

$$P = \rho g x \sin \beta + f(y, z)$$

but $p \neq p(y)$ as shown above, and we recognize that the pressure in gas above film is nearly constant at P_{atm} for short L , so at $x=0$, for all z , $P = P_{atm}$.

$$P = \rho g x \sin \beta + P_{atm}.$$

z -component eqn becomes.

$$\left[\frac{d}{dx} \tau_{xz} = \rho g \cos \beta \right]$$

(3.6-19)

(2.2-10)

See example 2.2-2

for solution when $\mu = \mu_0 e^{-\alpha x / \delta}$

$$\tau_z = \frac{\rho g \delta^2 \cos \beta}{2\mu} \left[1 - \left(\frac{x}{\delta} \right)^2 \right]$$

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