

# Michigan Tech

## CM3110 Morrison HW 6

### Answers to Assigned Problems:

1. See assignment. No answer provided (summary of data correlations). See lecture notes for an example.
2. Geankoplis 4.5-6:  $84 \text{ lb}_m/\text{h}$
3. Geankoplis 4.7-1:  $h = 5.4 \text{ W}/\text{m}^2$ ,  $q = 92 \text{ W}/\text{m}$  (not using the simplified equation);  $q = 85 \text{ W}/\text{m}$  (simplified equation)
4. Geankoplis 4.7-3:  $Q = 45 \text{ W}$
5. Geankoplis 4.5-4:  $T_1' = 299.5^\circ\text{C}$ ,  $A = 97 \text{ m}^2$  (assume double-pipe heat exchanger; note Geankoplis' use of an improbable number of sig figs)
6. Geankoplis 4.5-4, except with 1-2 shell-and-tube heat exchanger:  $T_1' = 299.5^\circ\text{C}$ ,  $A = 97 \text{ m}^2$ . How does the 1-2 shell-and-tube compare to the double pipe?
7. See assignment. Answers: a)  $26 \text{ kW}$ , b)  $\Delta T_{lm} = 63^\circ\text{C}$ ; c)  $U_o = 500 \text{ W}/\text{m}^2\text{K}$
8. See assignment. Answer:  $180 \text{ kW}$ .
9. Geankoplis 4.10-3:  $160 \text{ W}$
10. See assignment. Answer:  $260 \text{ W}$ . Neither radiation nor natural convection dominates.
11. Geankoplis 4.11-1: a)  $14,000 \text{ W}/\text{m}^2$ , b)  $4500 \text{ W}/\text{m}^2$
12. Geankoplis 4.7-8: We need to calculate radiation and natural convection contributions to the total. Answers: radiation  $5.5 \text{ kW}$ ; natural convection  $1.3 \text{ kW}$ ; total  $6.8 \text{ kW}$ .
13. See assignment. Answer: Only heat exchanger C will work.
14. See assignment. Answers: a)  $h_i = 6900 \frac{\text{W}}{\text{m}^2\text{K}}$ ,  $h_o = 2200 \text{ W}/\text{m}^2\text{K}$ ,  $U_o = 1400 \text{ W}/\text{m}^2\text{K}$  b) with water-side fouling  $U_o = 1100 \text{ W}/\text{m}^2\text{K}$ , with orange-juice side fouling,  $U_o = 900 \text{ W}/\text{m}^2\text{K}$ , with fouling on both sides,  $U_o = 800 \text{ W}/\text{m}^2\text{K}$
15. Problem N(stretch). Answer: b;  $h_{lm} = 5300 \frac{\text{W}}{\text{m}^2\text{K}}$ ,  $T = 21^\circ\text{C}$
16. Problem M. Answer: c; yes, radiation is important;  $h_{total} = 62 \frac{\text{W}}{\text{m}^2\text{K}}$ ;  $\frac{q}{A} = 6300 \text{ W}/\text{m}^2$
17. Problem K. Answer:  $h = 7.0 \frac{\text{W}}{\text{m}^2\text{K}}$ ,  $q = 130 \text{ W}$  (natural convection only)