

Introduction to McCabe-Thiele Design Method: Binary Distillation

PART I

~~★~~ PART II

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Ref: P. C. Wankat, *Separation Process Engineering*, Prentice Hall, 4th ed, 2017

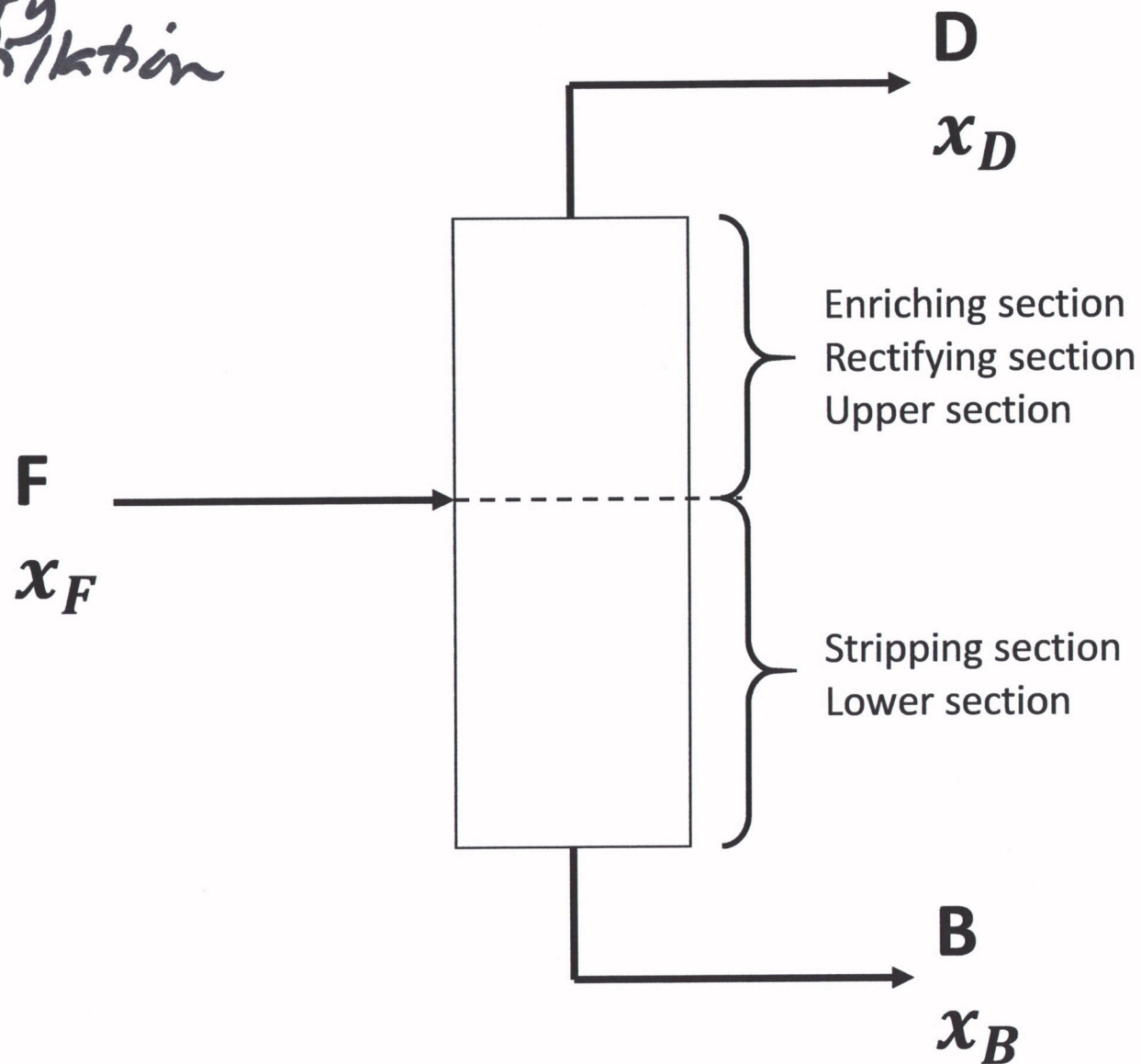
YouTube: DrMorrisonMTU

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McCabe-Thiele Method

Binary Distillation

McCabe-Thiele Method

The McCabe-Thiele method assumes

Constant Molar Overflow (CMO)

Enriching section

Liquid molar flow rates = L

Vapor molar flow rates = V

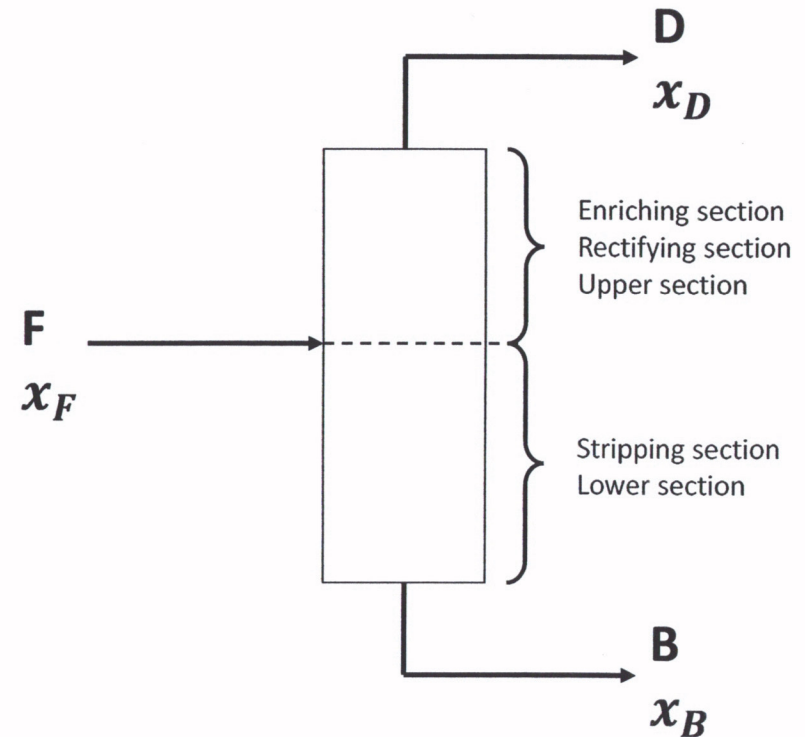
Stripping section

Liquid molar flow rates = $\bar{L}$

Vapor molar flow rates = $\bar{V}$

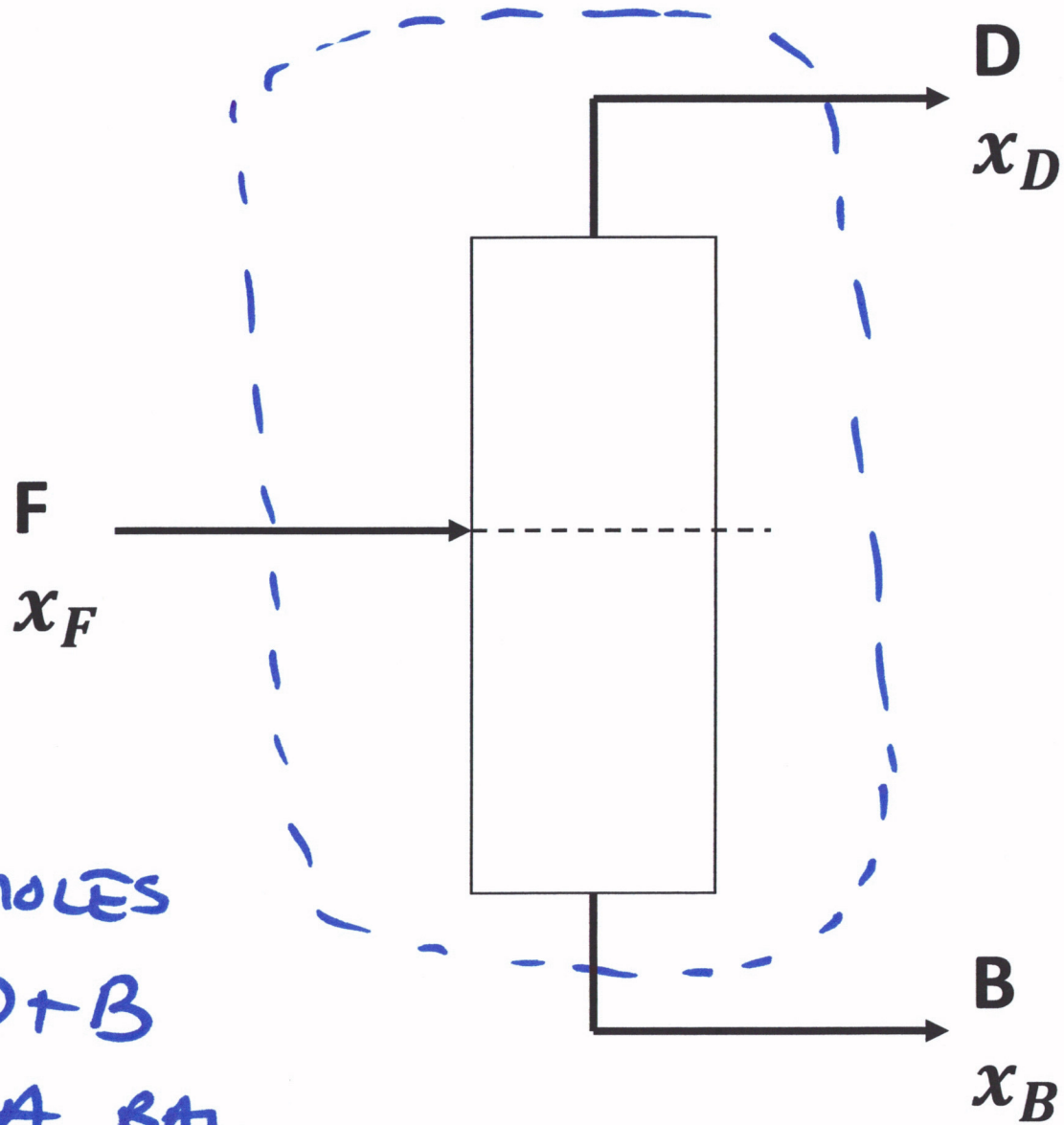
Four conditions:

1. $\Delta\hat{H}_{vap}$ independent of mixture concentration
2. Latent heat dominates
3. Adiabatic column, $\dot{Q} = 0$
4. Saturated liquid and vapor lines on $\hat{H} - x_A$ diagram are parallel



Overall mole balance

①



TOTAL MOLES

$$F = D + B$$

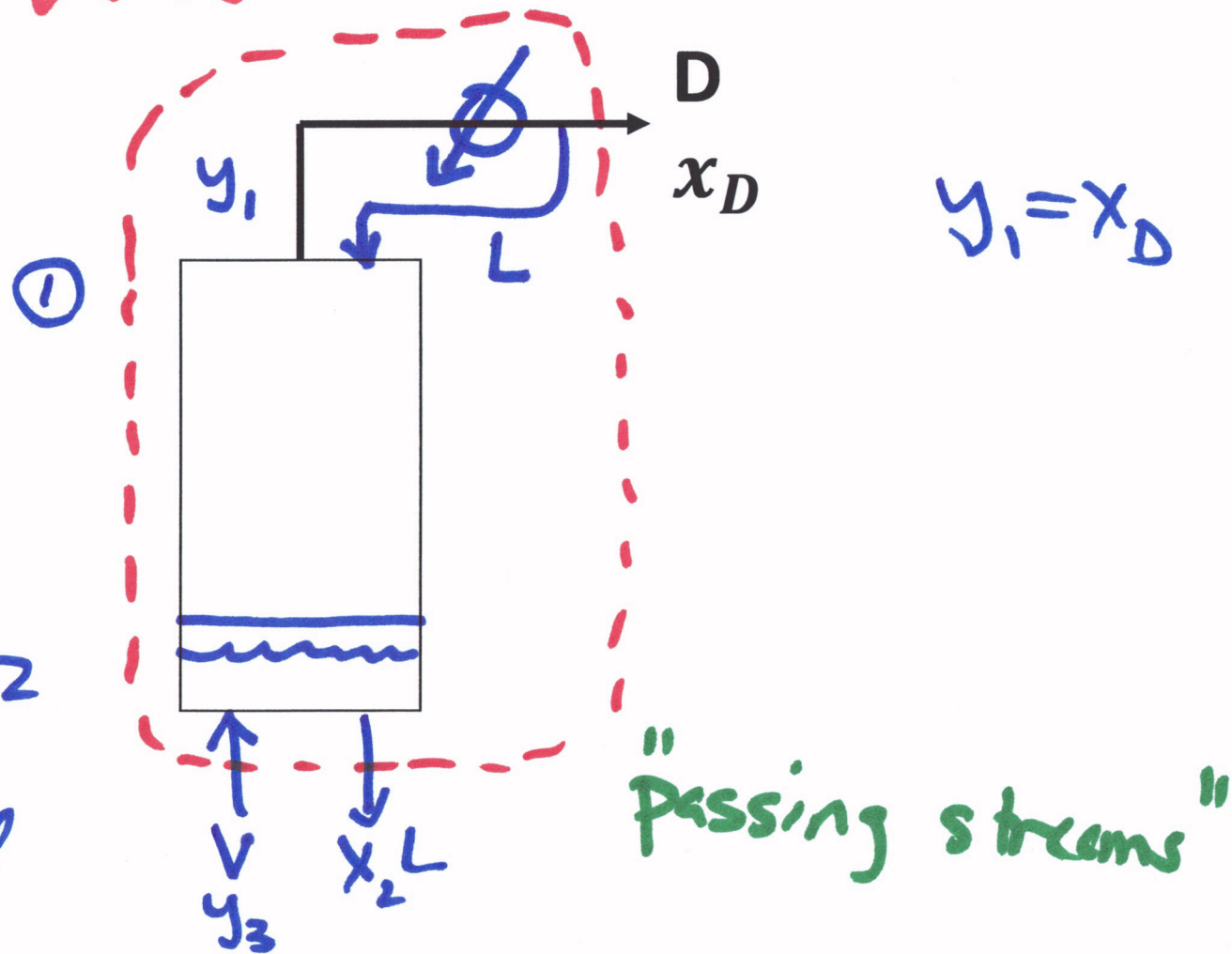
MOLES A BAL

$$x_F F = x_D D + x_B B$$

③

Mass balance (molar basis) Enriching Section

total condenser



total molar bal

$$V = L + D$$

molar A bal

$$\# y_3 V = x_2 L + x_D D$$

$$y_3 = \left(\frac{L}{V}\right) x_2 + \frac{D}{V} x_D \quad \leftarrow = V-L$$

$$y_3 = \left(\frac{L}{V}\right) x_2 + \left(\frac{V-L}{V}\right) x_D$$

$$\boxed{y = \underbrace{\left(\frac{L}{V}\right)}_{\text{slope}} x + \left(1 - \frac{L}{V}\right) x_D}$$

operating line (enriching section)

To find a point on
the line

$$\text{Let } x = x_D$$

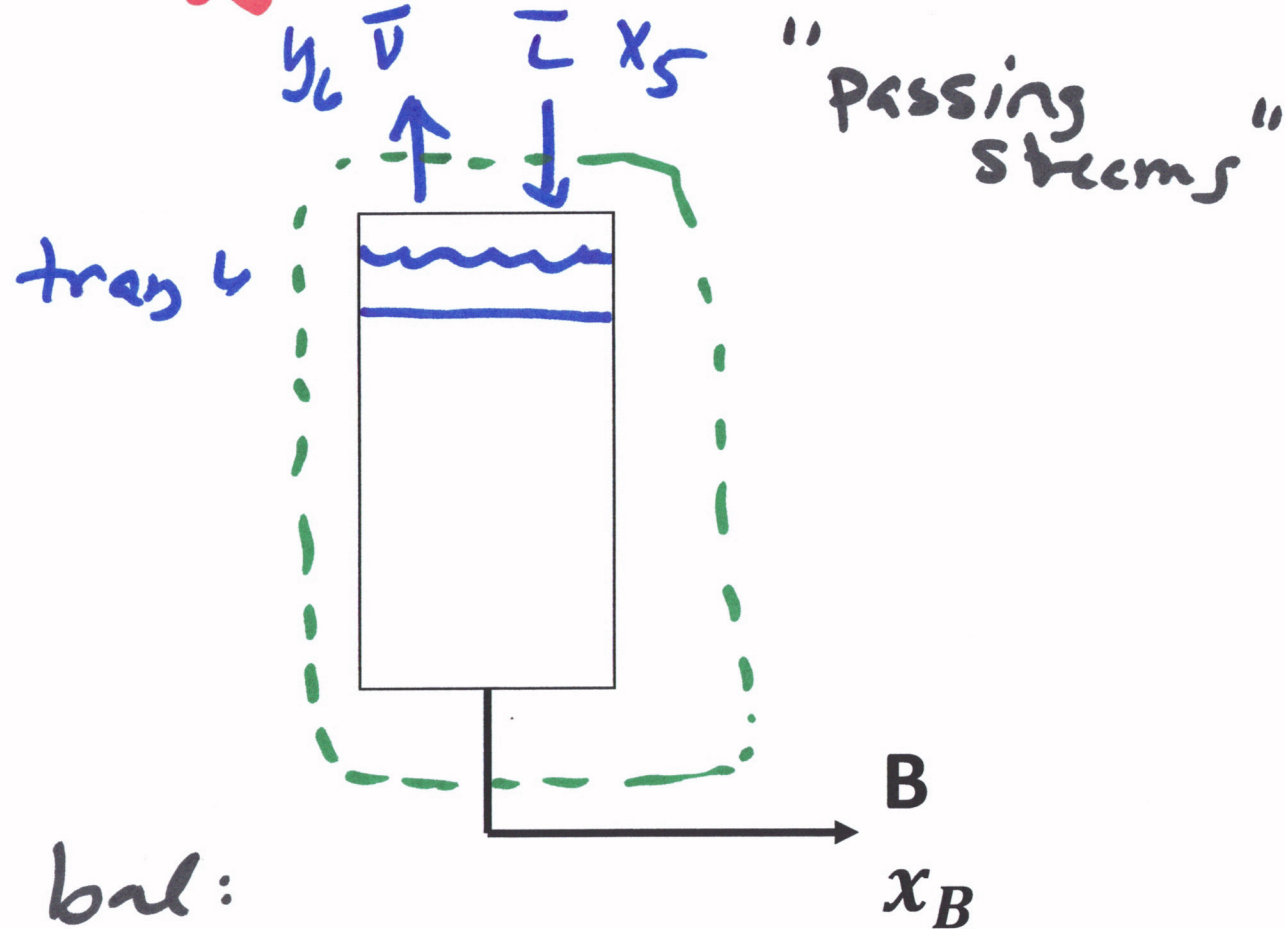
$$y = \frac{L}{V} x_D + (1 - \frac{L}{V}) x_D$$

$$= \cancel{\frac{L}{V} x_D} + x_D - \cancel{(\frac{L}{V}) x_D}$$

$$\boxed{y = x_D}$$

④

Mass balance (molar basis) Stripping Section



total mol bal:

$$\bar{L} = \bar{V} + B$$

mass A bal:

$$x_5 \bar{L} = y_4 \bar{V} + x_B B$$

★

$$\rightarrow y_L \bar{V} = x_S \bar{L} - x_B B$$

⑤

$$y_L = \left(\frac{\bar{L}}{\bar{V}} \right) x_S - \left(\frac{B}{\bar{V}} \right) x_B \quad \bar{L} - \bar{V}$$

$$y_L = \left(\frac{\bar{L}}{\bar{V}} \right) x_S - \left(\frac{\bar{L} - \bar{V}}{\bar{V}} \right) x_B$$

$$\boxed{\bar{y} = \left(\frac{\bar{L}}{\bar{V}} \right) \bar{x} - \left(\frac{\bar{L}}{\bar{V}} - 1 \right) x_B}$$

operating line
(stripping section)

To find a point on the line →

$$\text{Let } \bar{x} = x_B$$

$$\bar{y} = \left(\frac{\bar{L}}{\bar{V}} \right) x_B - \left(\frac{\bar{L}}{\bar{V}} - 1 \right) x_B$$

$$= \cancel{\left(\frac{\bar{L}}{\bar{V}} \right) x_B} - \cancel{\left(\frac{\bar{L}}{\bar{V}} x_B \right)} + x_B$$

$$\boxed{\bar{y} = x_B}$$

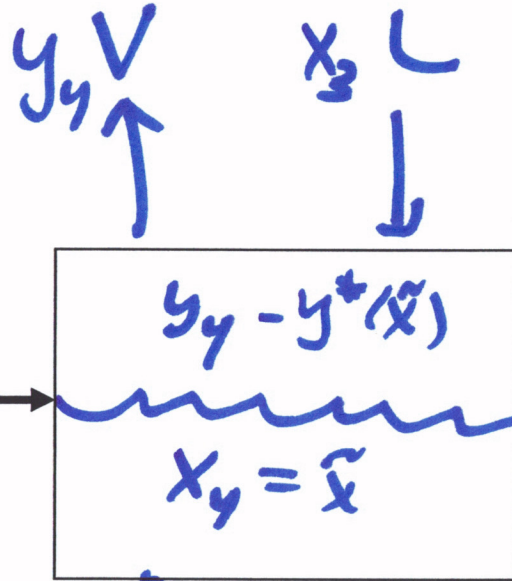
⑥

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Feed Tray

stage 4

F
 x_F



$\tilde{x} \neq \tilde{y}$
are passing
streams

(top + bottom)

$$\tilde{y} = y_5 \bar{V}$$

$$\bar{L} \downarrow$$

$$x_4 = \tilde{x}$$

AT FEED

⑧

★ ① $\tilde{y} \bar{v} = \tilde{x} \bar{l} - x_B B$ stripping

★ ② $\tilde{y} v = \tilde{x} L + x_D D$ enriching

subtract ② - ①

$$\tilde{y} (v - \bar{v}) = \tilde{x} (L - \bar{l}) + \overbrace{x_D D + x_B B}^{x_P F}$$

$$\tilde{y} = \left(\frac{L - \bar{l}}{v - \bar{v}} \right) \tilde{x} + \frac{x_P F}{v - \bar{v}}$$

"passing streams"
(at feed tray)

To find a point
on the fed line →

$$\text{let } \tilde{x} = x_F$$

$$\tilde{y} = \left(\frac{L - \bar{L}}{V - \bar{V}} \right) x_F + \frac{x_F F}{V - \bar{V}}$$

(return to this
after quality
discussion)

Returning (see p11)

$$\tilde{y} = \left(\frac{-gF}{(1-g)F} \right) x_F + \frac{x_F F}{(1-g)F}$$

$$\tilde{y} = \left(-\frac{g}{1-g} \right) x_F + \left(\frac{1}{1-g} \right) x_f$$

⑨

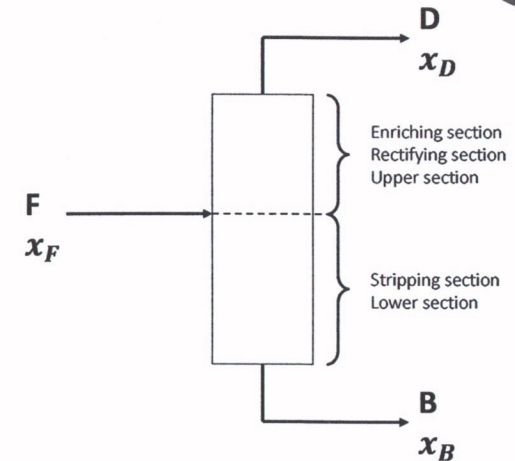
$$\tilde{y} = \frac{(1-\cancel{s})X_F}{(1-\cancel{s})}$$

$$\boxed{\tilde{y} = X_F}$$

9½

(the third time
we found a point
on the 45° line)

Goal: Determine the number of stages of a distillation column that can achieve the desired separation



Constraints

1. Overall mass conservation (mole balances)
2. Equilibrium stages $y^* (x^*)$
3. All stages above the feed satisfy the same mole balances drawn through D
4. All stages below the feed satisfy the same mole balances drawn through B
5. Upper and lower operating lines intersect at the feed tray
6. The quality q of the feed and mole balances on each phase at the feed tray close the calculation

→
Now



Summary of Constraints (thus far)

1. Overall mass conservation (mole balances)

$$V = L + D$$

$$x_F F = x_D D + x_B B$$

1. Equilibrium stages: data $y^* = f(x^*)$
2. Above the feed mole balances constrain passing streams $y(x)$ (operating line):

$$y = \left(\frac{L}{V}\right)x + \left(1 - \frac{L}{V}\right)x_D$$

3. Below the feed passing streams $\bar{y}(\bar{x})$ (operating line)

$$\bar{y} = \left(\frac{\bar{L}}{\bar{V}}\right)\bar{x} - \left(\frac{\bar{L}}{\bar{V}} - 1\right)x_B$$

5. Upper and lower intersect at feed tray, $\tilde{y}(\tilde{x})$

$$\tilde{y} = \left(\frac{L - \bar{L}}{V - \bar{V}}\right)\tilde{x} + \frac{x_F F}{V - \bar{V}}$$

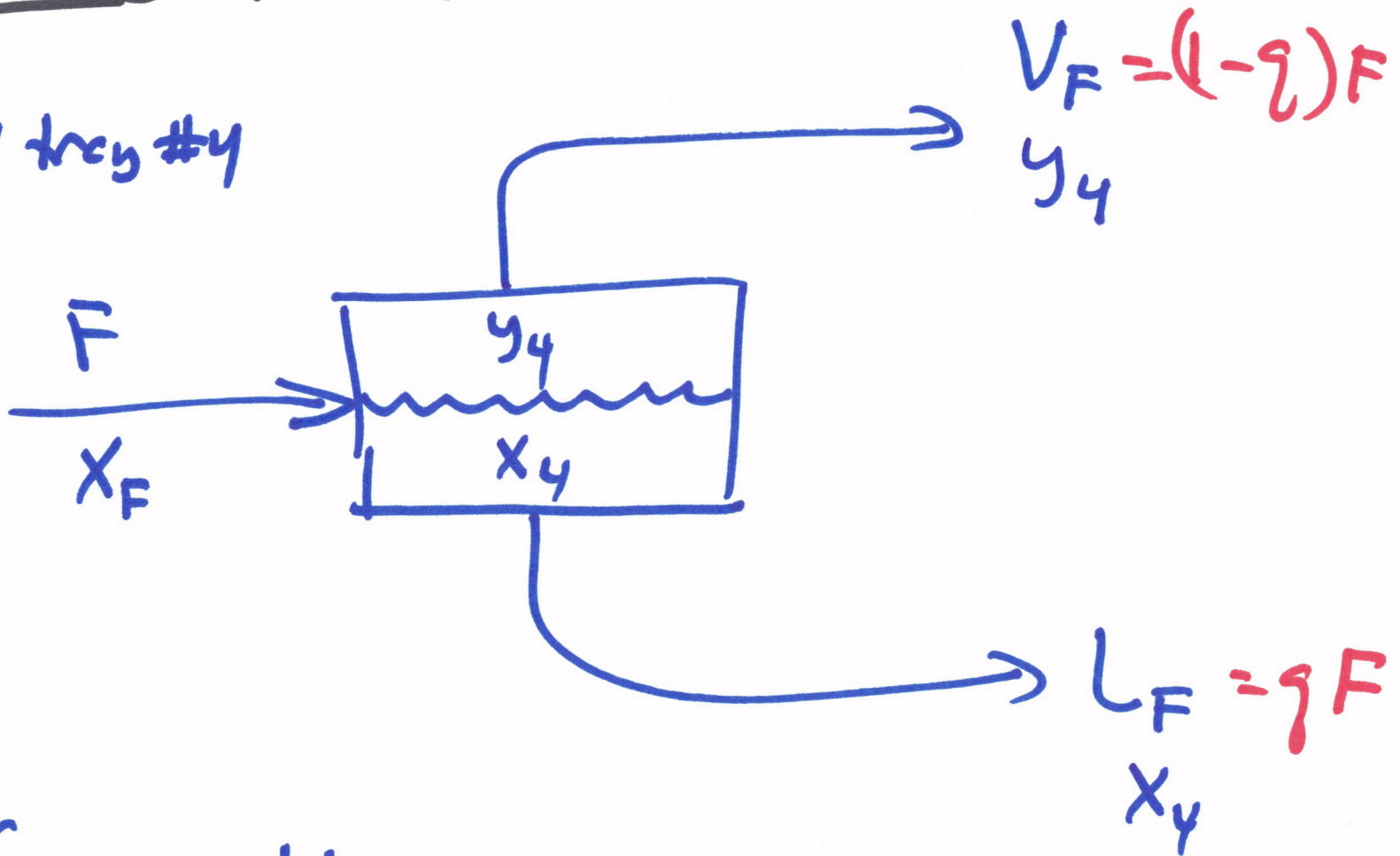
4. The quality q of the feed and mole balances on each phase at the feed tray close the calculation

$$-qF = L - \bar{L}; (1-q)F = V - \bar{V}; \tilde{y} = \left(\frac{q}{q-1}\right)\tilde{x} + \frac{x_F}{1-q}$$

Quality of feed

(10)

feed tray #4

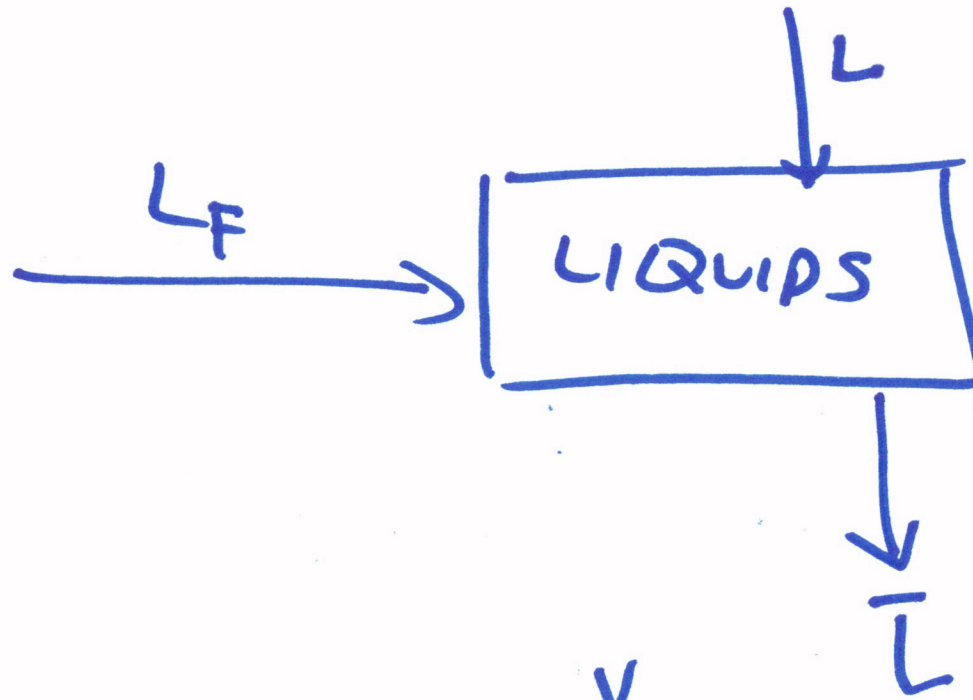


define quality:

$$g = \frac{L_F}{F}$$

$$1 - g = \frac{F - L_F}{F} = \frac{V_F}{F}$$

①

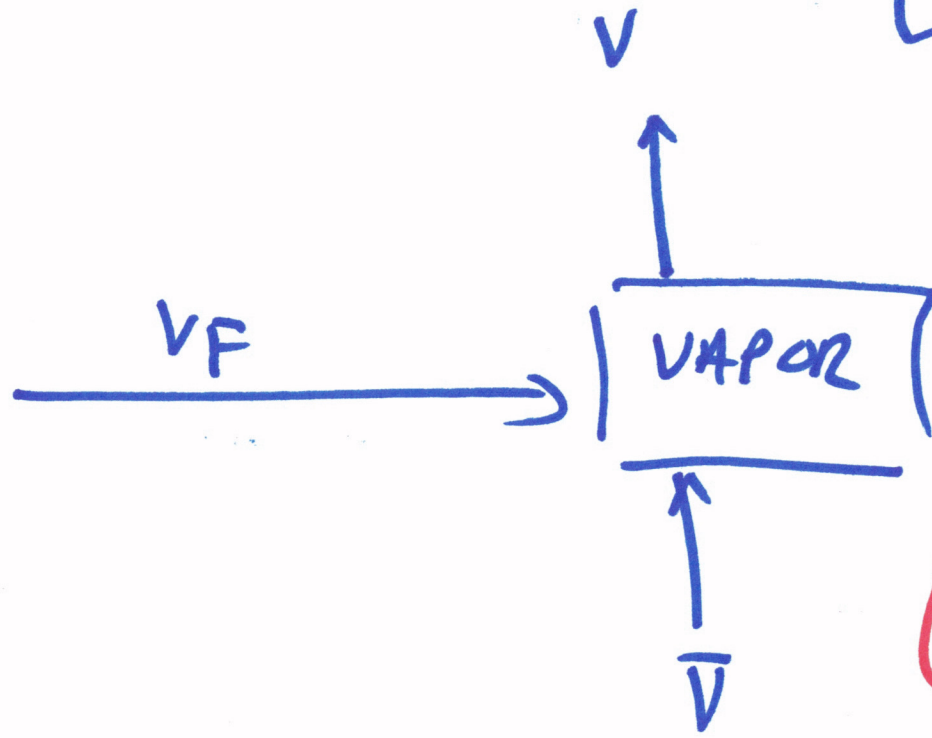


$$L_F + L = \bar{L}$$

$$L_F = \bar{L} - L$$

$$-L_F = L - \bar{L}$$

$$\boxed{-qF = L - \bar{L}}$$



$$V_F + \bar{V} = V$$

$$V_F = V - \bar{V}$$

$$\boxed{(1-q)F = V - \bar{V}}$$

Returning to the feed tray:
(passing streams)

(12)

$$\tilde{y} = \underbrace{\left(\frac{L - \bar{L}}{V - \bar{V}} \right)}_{(1-g)K} \tilde{x} + \frac{x_F \cancel{F}}{\underbrace{V - \bar{V}}_{(1-g)K}}$$

$$\tilde{y} = \left(\frac{-g}{1-g} \right) \tilde{x} + \left(\frac{x_F}{1-g} \right)$$

$$\tilde{y} = \underbrace{\left(\frac{g}{g-1} \right)}_{\text{slope}} \tilde{x} + \frac{x_F}{1-g}$$

g -line
(feed)

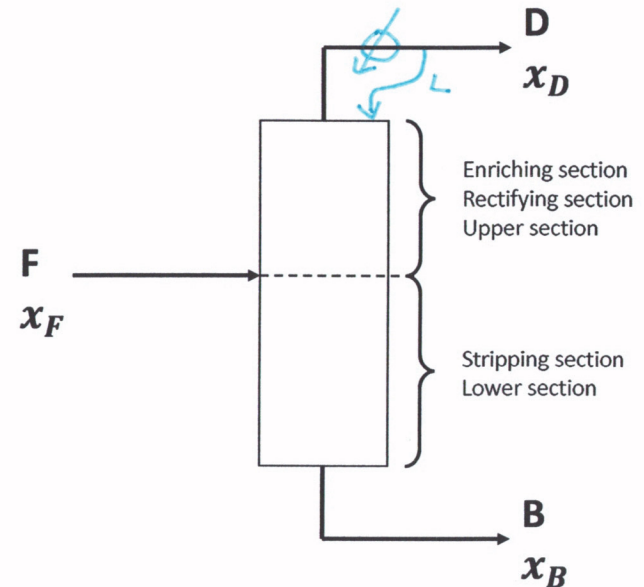
McCabe-Thiele Design Calculation—Binary Distillation

Find:

1. Number of equilibrium stages
2. Optimum location of the feed

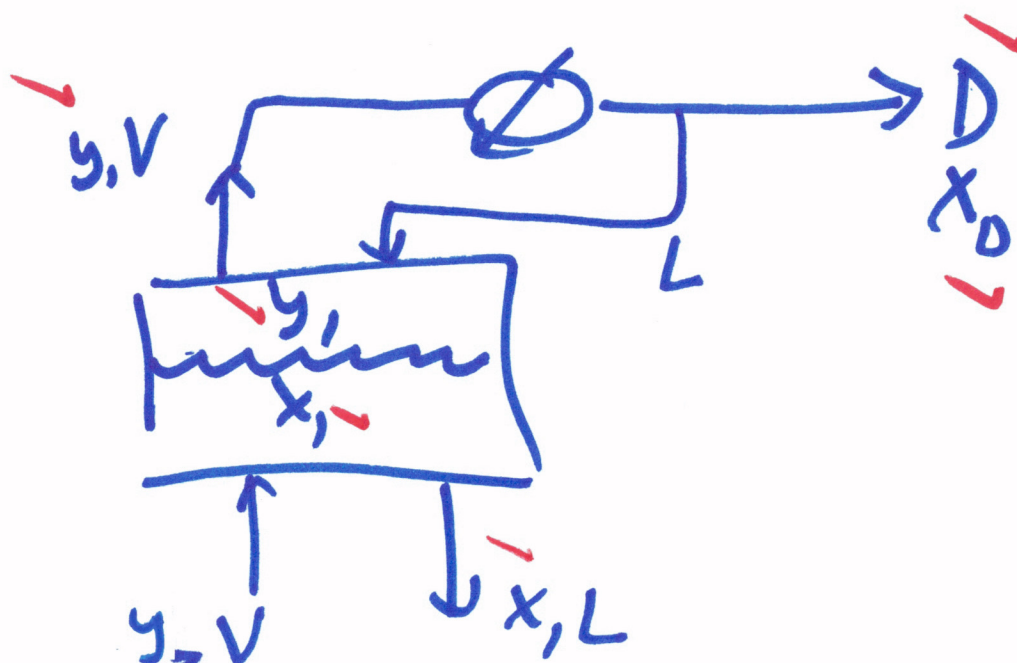
Given:

1. F, x_F, x_D, x_B
2. Column pressure (sets $y^*(x^*)$)
3. $q = 0.5$ *slope -1*
4. Reflux ratio, $r = \frac{L}{V} = 0.625$

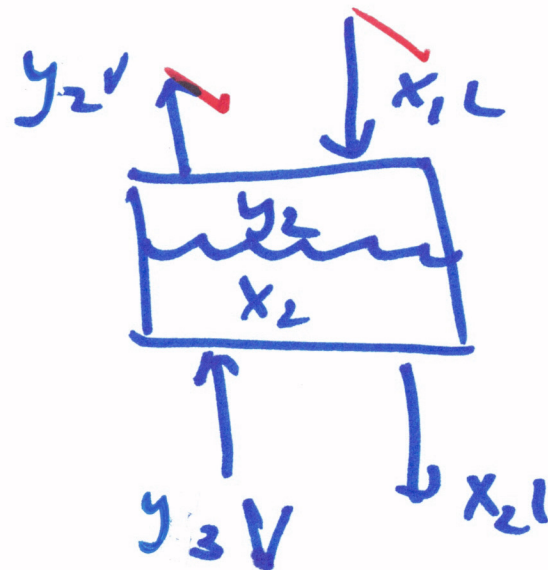


Walk
thru
column...

Stage 1



Stage 2



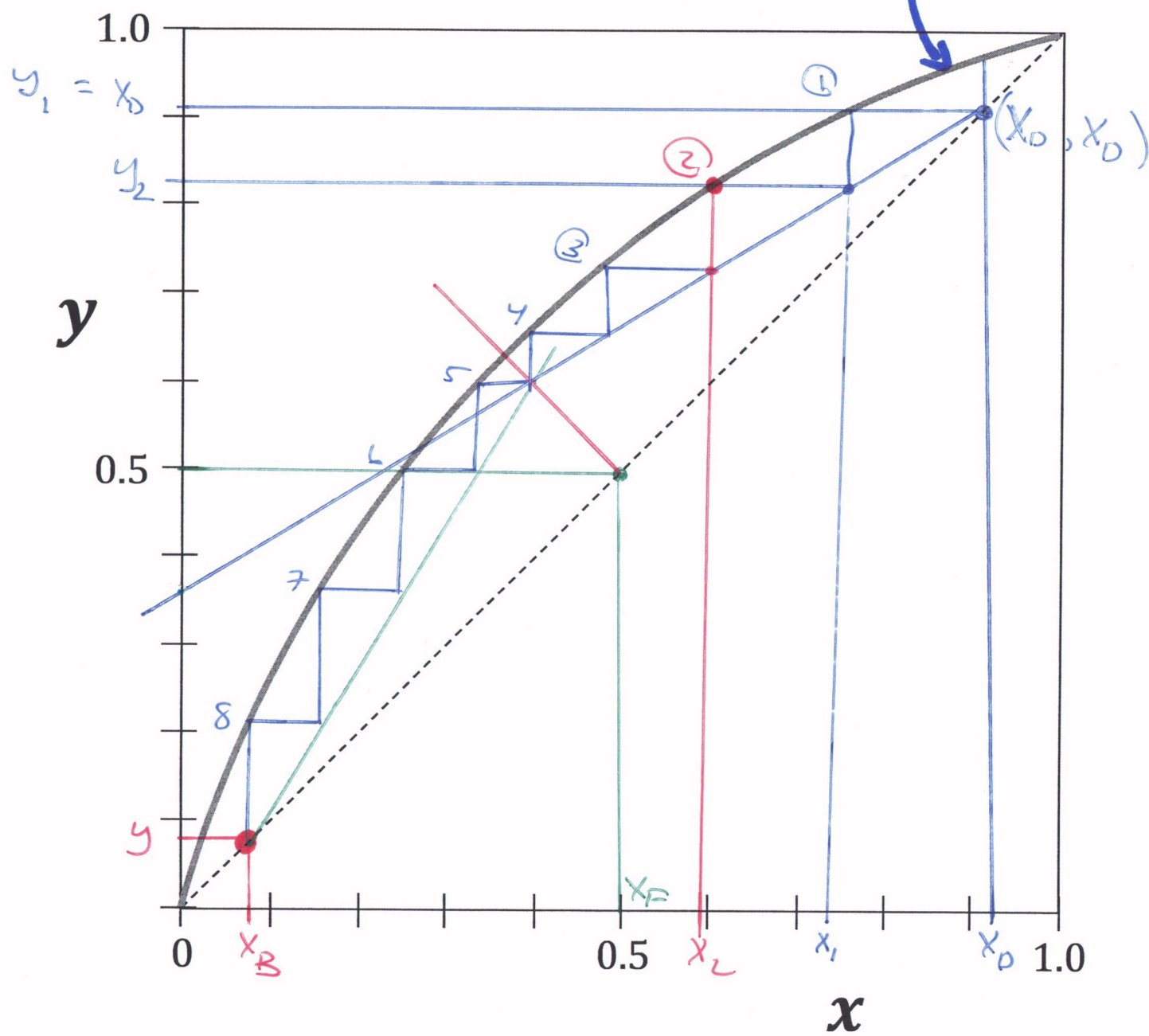
etc.

$$\frac{L}{V} = 0.625$$

(reflux ratio)

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(5)



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