

## The Heat/Mass Transfer Analogy

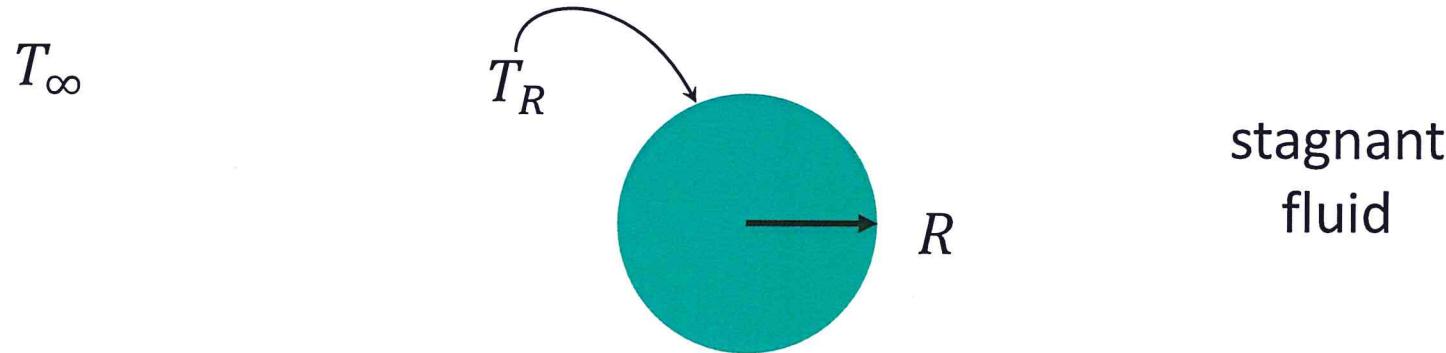
**heat**

**Example:** A spherical pellet of reacting solid slowly emits heat steadily into a stagnant fluid such that the surface temperature is constant. What is the heat transfer coefficient  $h$ ? What is the Nusselt number for this situation?

## Routes to Mass Transfer Correlations

**Theoretical**

- Based on a model of the situation; can be solved for flux, and thus for  $k_x$
- All models have assumptions; how good the assumptions are determine how good the correlations are
- The heat-transfer analogy counts as a theoretical pathway



# Solve.

N

## The Equation of Energy for systems with constant $k$

**Microscopic energy balance, constant thermal conductivity; Gibbs notation**

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + \underline{y} \cdot \nabla T \right) = k \nabla^2 T + S$$

**Microscopic energy balance, constant thermal conductivity; Cartesian coordinates**

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_x \frac{\partial T}{\partial x} + v_y \frac{\partial T}{\partial y} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + S$$

**Microscopic energy balance, constant thermal conductivity; cylindrical coordinates**

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right) = k \left( \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right) + S$$

**Microscopic energy balance, constant thermal conductivity; spherical coordinates**

no axial symmetry

$$\rho C_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi} \right) = k \left( \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial}{\partial \phi} \left( \frac{\partial T}{\partial \phi} \right) \right)$$

$v_r = 0$

$\theta, \phi$  symmetry

$\phi = \phi(r)$

$\theta = \theta(r)$

$T = T(r)$

- cosine

Reference: F. A. Morrison, "Web Appendix to *An Introduction to Fluid Mechanics*," Cambridge University Press, New York, 2013. On the web at [www.chem.mtu.edu/~fmorriso/EM\\_WebAppendixCD2013.pdf](http://www.chem.mtu.edu/~fmorriso/EM_WebAppendixCD2013.pdf)

$$\frac{d\bar{\Phi}}{dr} = 0$$

integrate:

$$\bar{\Phi} = C_1 = r^2 \frac{dT}{dr}$$

integrate:  $\frac{dT}{dr} = \frac{G}{r^2}$

$$T = -\frac{C_1}{r} + C_2$$

B.C.:  $r=R \quad T=T_R$   
 $r=\infty \quad T=T_\infty$

or could  
use Newton's  
law of  
cooling -  
both work in  
this  
problem

④

Substituting  
the  
B.C.

$$\left\{ \begin{array}{l} T_R = -\frac{C_1}{R} + C_L \\ T_\infty = C_2 \end{array} \right.$$

$$C_1 = -(T_R - T_\infty) R \quad |$$

$$T = \frac{(T_R - T_\infty) R}{r} + T_\infty \quad |$$

Final temperature  
distribution

match flux at  $r=R$ :

(3)

$$h(\bar{T}_R - \bar{T}) = \left( -k \frac{dT}{dr} \right) \Big|_{r=R}$$
$$\frac{c_1}{r^2} \Big|_{r=R}$$

$$h(\bar{T}_R - \bar{T}) = -\frac{k}{R^2} (-)(\bar{T}_R - \bar{T}) R$$

multiply by  $2R$ :

diameter  $\rightarrow$

$$N_u \equiv \frac{hD}{k}$$
$$D = 2R$$

$$(2R) h = \frac{k}{R} (2R) \quad N_u = \frac{h/(2R)}{k}$$

$$N_u = \frac{h/(2R)}{k} = 2 \quad |$$

(6)

## The **Equation of Energy** in Cartesian, cylindrical, and spherical coordinates for

Newtonian fluids of constant density, with source term  $S$ . Source could be electrical energy due to current flow, chemical energy, etc. Two cases are presented: the general case where thermal conductivity may be a function of temperature (vector flux  $\underline{\tilde{q}} = \underline{q}/A$  appears in the equations); and the more usual case, where thermal conductivity is constant.

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**Microscopic energy balance**, in terms of flux; Gibbs notation

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + \underline{v} \cdot \nabla T \right) = -\nabla \cdot \underline{\tilde{q}} + S$$

**Microscopic energy balance**, in terms of flux; Cartesian coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_x \frac{\partial T}{\partial x} + v_y \frac{\partial T}{\partial y} + v_z \frac{\partial T}{\partial z} \right) = - \left( \frac{\partial \tilde{q}_x}{\partial x} + \frac{\partial \tilde{q}_y}{\partial y} + \frac{\partial \tilde{q}_z}{\partial z} \right) + S$$

**Microscopic energy balance**, in terms of flux; cylindrical coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + v_z \frac{\partial T}{\partial z} \right) = - \left( \frac{1}{r} \frac{\partial (r \tilde{q}_r)}{\partial r} + \frac{1}{r} \frac{\partial \tilde{q}_\theta}{\partial \theta} + \frac{\partial \tilde{q}_z}{\partial z} \right) + S$$

**Microscopic energy balance**, in terms of flux; spherical coordinates

$$\rho \hat{C}_p \left( \frac{\partial T}{\partial t} + v_r \frac{\partial T}{\partial r} + \frac{v_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi} \right) = - \left( \frac{1}{r^2} \frac{\partial (r^2 \tilde{q}_r)}{\partial r} + \frac{1}{r \sin \theta} \frac{\partial (\tilde{q}_\theta \sin \theta)}{\partial \theta} + \frac{1}{r \sin \theta} \frac{\partial (\tilde{q}_\phi)}{\partial \phi} \right) + S$$

**Fourier's law of heat conduction**, Gibbs notation:  $\underline{\tilde{q}} = -k \nabla T$

$$\text{Fourier's law of heat conduction, Cartesian coordinates: } \begin{pmatrix} \tilde{q}_x \\ \tilde{q}_y \\ \tilde{q}_z \end{pmatrix}_{xyz} = \begin{pmatrix} -k \frac{\partial T}{\partial x} \\ -k \frac{\partial T}{\partial y} \\ -k \frac{\partial T}{\partial z} \end{pmatrix}_{xyz}$$

$$\text{Fourier's law of heat conduction, cylindrical coordinates: } \begin{pmatrix} \tilde{q}_r \\ \tilde{q}_\theta \\ \tilde{q}_z \end{pmatrix}_{xyz} = \begin{pmatrix} -k \frac{\partial T}{\partial r} \\ -k \frac{\partial T}{\partial \theta} \\ -k \frac{\partial T}{\partial z} \end{pmatrix}_{r\theta z}$$

$$\text{Fourier's law of heat conduction, spherical coordinates: } \begin{pmatrix} \tilde{q}_r \\ \tilde{q}_\theta \\ \tilde{q}_\phi \end{pmatrix}_{xyz} = \begin{pmatrix} -k \frac{\partial T}{\partial r} \\ -k \frac{\partial T}{\partial \theta} \\ -k \frac{\partial T}{\partial \phi} \end{pmatrix}_{r\theta\phi}$$

The flux in liquid