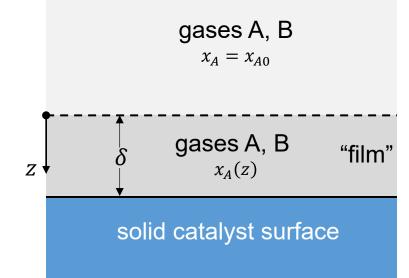
EXAMPLE 3: 26FEB2020

Film model of mass transfer (more complex)

Example 3: Heterogeneous catalysis

An irreversible, instantaneous chemical reaction $(2A \rightarrow B)$ takes place at a catalyst surface, as shown. The reaction is "diffusion-limited," however, because the rate of completion of the reaction is determined by the rate of diffusion through the "film" near the catalyst surface. Calculate the steady state composition distribution in the film $x_A(z)$ and the flux of product *B* away from the surface.



- Deploy the "film model"
- It has become a way of thinking about diffusion in some circumstances

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model 3 GAS A, B I (inert) (isnon) XAO CATALYST SUPPORT How Can we model this reacher? (reflect!) 2A → B ·at surface .fast . irrunsible Use micro, species A mets bal . assuming diffind

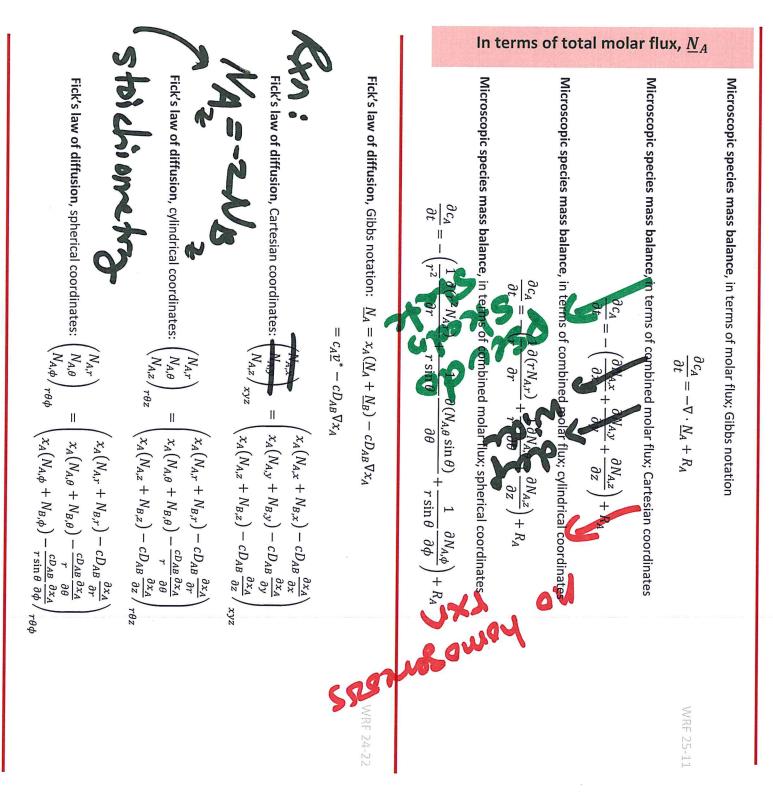


The Equation of Species Mass Balance in Terms of Combined

Alolar quantities in Cartesian, cylindrical, and spherical coordinates for binary mixtures of A and B.

The general case, where the combined molar flux with respect to molar velocity (N_A), is given on page 1.

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Micro Species A Mass balence: Ø $\frac{dN_{A,z}}{dz} = 0$ $inksrak: N_{A_{12}} = C_{1}$ assumetant cDAB Fick is Lew A Diffusion: $N_{A,z} = X_A (N_{A_z} + N_{B_z}) - c D_{AB} \frac{dX_A}{dz}$ - z NA, z (from stoichiometry)



 $N_{AZ} = X_A \left(\frac{t}{z}\right) N_{AZ} - c D_{AB} \frac{d X_A}{d Z}$ $(1 - \frac{x_{A}}{2}) N_{A_{z}} = -CD_{AB} \frac{dx_{A}}{dz}$ Solve for XA w/ Z Boundary Conditions Boundary Conditions: 2=0 X = XAO XA=O E it Hads! 5-2 (Su HWY Solns) //