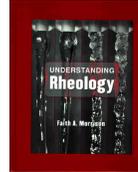


Polymer Rheology

Rhe-

$\rho\epsilon\iota$ – Greek for flow

CM4650 Polymer
Rheology
Michigan Tech



What is rheology anyway?

*Rheology = the study of
deformation and flow.*

“What is Rheology Anyway?” Faith
A. Morrison, *The Industrial Physicist*,
10(2) 29-31, April/May 2004.

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What is rheology anyway?

To the layperson, rheology is

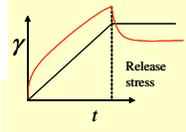
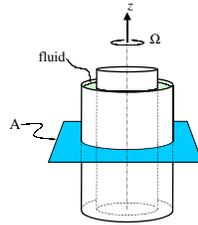


- Mayonnaise does not flow even under stress for a long time; honey always flows
- Silly Putty bounces (is elastic) but also flows (is viscous)
- Dilute flour-water solutions are easy to work with but doughs can be quite temperamental
- Corn starch and water can display strange behavior – poke it slowly and it deforms easily around your finger; punch it rapidly and your fist bounces off of the surface

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What is rheology anyway?

To the scientist, engineer, or technician, rheology is



- Yield stresses
- Viscoelastic effects
- Memory effects
- Shear thickening and shear thinning

For both the layperson and the technical person, rheology is a set of problems or observations related to how the stress in a material or force applied to a material is related to deformation (change of shape) of the material.

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What is rheology anyway?

Rheology affects:



- End use (food texture, product pour, motor-oil function)

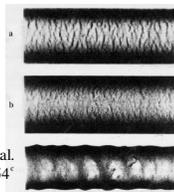
- Processing (design, costs, production rates)



www.corrugatorman.com/pic/akron%20extruder.JPG



www.math.utwente.nl/mpcm/aamp/examples.html



Pomar et al.
JNNFM 54^c
143 1994

- Product quality (surface distortions, anisotropy, strength, structure development)

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Goal of the scientist, engineer, or technician:

- **Understand** the kinds of flow and deformation **effects** exhibited by complex systems
- **Apply qualitative** rheological **knowledge** to diagnostic, design, or optimization problems
- In diagnostic, design, or optimization problems, **use or devise quantitative** analytical **tools** that correctly capture rheological effects

**How
do we reach
these goals?**

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How?

By observing the behavior
of different systems

• **Understand** the kinds of flow and deformation **effects** exhibited by complex systems

• **Apply qualitative** rheological **knowledge** to diagnostic, design, or optimization problems

• In diagnostic, design, or optimization problems, **Use or devise quantitative** analytical **tools** that correctly capture rheological effects

By making
calculations
with models in
appropriate
situations

By learning
which
quantitative
models
apply in
what
circum-
stances

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Learning Rheology (bibliography)

Descriptive Rheology

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Quantitative Rheology

Morrison, Faith, *Understanding Rheology* (Oxford, 2001)
Bird, R., R. Armstrong, and O. Hassager, *Dynamics of Polymeric Liquids, Volume 1* (Wiley, 1987)

Industrial Rheology

Dealy, John and Kurt Wissbrun, *Melt Rheology and Its Role in Plastics Processing* (Van Nostrand Reinhold, 1990)

Polymer Behavior

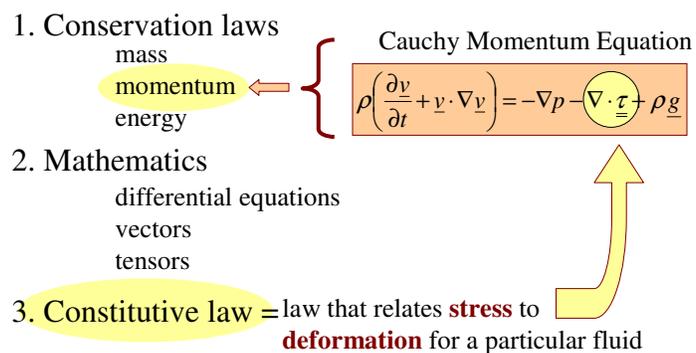
Larson, Ron, *The Structure and Rheology of Complex Fluids* (Oxford, 1999)
Ferry, John, *Viscoelastic Properties of Polymers* (Wiley, 1980)

Suspension Behavior

Larson, Ron, *The Structure and Rheology of Complex Fluids* (Oxford, 1999)
Macosko, Chris, *Rheology: Principles, Measurements, and Applications* (VCH Publishers, 1994)

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The Physics Behind Rheology:



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Newtonian fluids:
(fluid mechanics)

$$\tau_{21} = -\mu \frac{dv_1}{dx_2}$$

material parameter

deformation

Newton's Law of Viscosity

- This is an empirical law (measured or observed)
- May be derived theoretically for some systems

Non-Newtonian fluids:
(rheology)

Need a new law or new laws

- These laws will also either be empirical or will be derived theoretically

Newtonian fluids:
(shear flow only)

$$\tau_{21} = -\mu \frac{dv_1}{dx_2}$$

Constitutive Equation

Non-Newtonian fluids:
(all flows)

$$\underline{\underline{\tau}} = -f(\underline{\underline{\dot{\gamma}}})$$

stress tensor

Rate-of-deformation tensor

non-linear function (in time and position)

Introduction to Non-Newtonian Behavior

*Rheological Behavior of Fluids, National
Committee on Fluid Mechanics Films, 1964*

Velocity gradient tensor $\underline{\dot{\gamma}}$

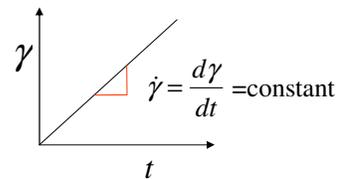
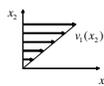
Type of fluid	Momentum balance	Stress –Deformation relationship (constitutive equation)
Inviscid (zero viscosity, $\mu=0$)	Euler equation (Navier-Stokes with zero viscosity)	Stress is isotropic
Newtonian (finite, constant viscosity, μ)	Navier-Stokes (Cauchy momentum equation with Newtonian constitutive equation)	Stress is a function of the instantaneous velocity gradient
Non-Newtonian (finite, variable viscosity η plus memory effects)	Cauchy momentum equation with memory constitutive equation	Stress is a function of the history of the velocity gradient

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Rheological Behavior of Fluids - **Newtonian**

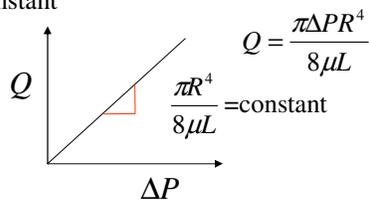
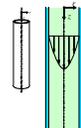
1. Strain response to imposed shear stress

•shear rate is constant



2. Pressure-driven flow in a tube (Poiseuille flow)

•viscosity is constant



3. Stress tensor in shear flow

•only two components are nonzero



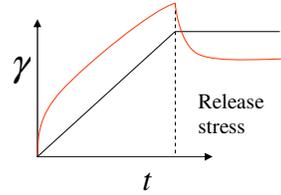
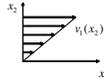
$$\underline{\underline{\tau}} = \begin{pmatrix} 0 & \tau_{12} & 0 \\ \tau_{21} & 0 & 0 \\ 0 & 0 & 0 \end{pmatrix}_{123}$$

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Rheological Behavior of Fluids – non-Newtonian

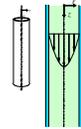
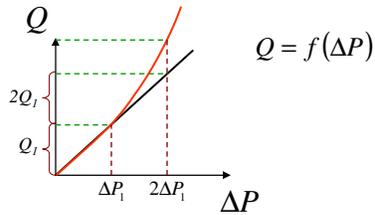
1. Strain response to imposed shear stress

- shear rate is variable



2. Pressure-driven flow in a tube (Poiseuille flow)

- viscosity is variable



3. Stress tensor in shear flow

Normal stresses

- all 9 components are nonzero



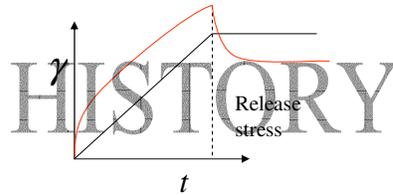
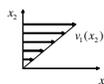
$$\underline{\underline{\tau}} = \begin{pmatrix} \tau_{11} & \tau_{12} & \tau_{13} \\ \tau_{21} & \tau_{22} & \tau_{23} \\ \tau_{31} & \tau_{32} & \tau_{33} \end{pmatrix}_{123}$$

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Rheological Behavior of Fluids – non-Newtonian

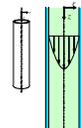
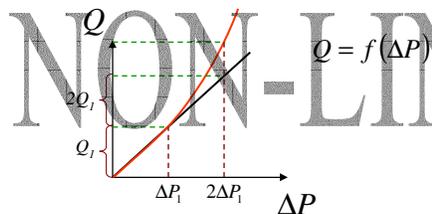
1. Strain response to imposed shear stress

- shear rate is variable



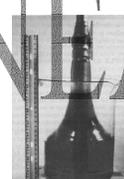
2. Pressure-driven flow in a tube (Poiseuille flow)

- viscosity is variable



Normal stresses

- all 9 components are nonzero



$$\underline{\underline{\tau}} = \begin{pmatrix} \tau_{11} & \tau_{12} & \tau_{13} \\ \tau_{21} & \tau_{22} & \tau_{23} \\ \tau_{31} & \tau_{32} & \tau_{33} \end{pmatrix}_{123}$$

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Examples from the film of

Dependence on the history of the deformation gradient

- Polymer fluid pours, but springs back
- Elastic ball bounces, but flows if given enough time
- Steel ball dropped in polymer solution “bounces”
- Polymer solution in concentric cylinders – has fading memory
- Quantitative measurements in concentric cylinders show memory and need a finite time to come to steady state

Non-linearity of the function $\underline{\tau} = f(\underline{\dot{\gamma}})$

- Polymer solution draining from a tube is first slower, then faster than a Newtonian fluid
- Double the static head on a draining tube, and the flow rate does not necessarily double (as it does for Newtonian fluids); sometimes more than doubles, sometimes less
- Normal stresses in shear flow
- Die swell

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**Show NCFM Film
on *Rheological
Behavior of Fluids***

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